



(12) **United States Patent**
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(54) **ACOUSTOPHORETIC DEVICE WITH
PIEZOELECTRIC TRANSDUCER ARRAY**

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patent is extended or adjusted under 35
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B01D 43/00 (2006.01)
H01L 41/053 (2006.01)
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CPC **B01D 43/00** (2013.01); **B06B 1/06**
(2013.01); **C12M 47/02** (2013.01); **H01L**
41/0533 (2013.01)

(58) **Field of Classification Search**
CPC B01D 29/115; B01D 37/00; B01D 29/52;
C21B 3/04

See application file for complete search history.

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Primary Examiner — Walter D Griffin

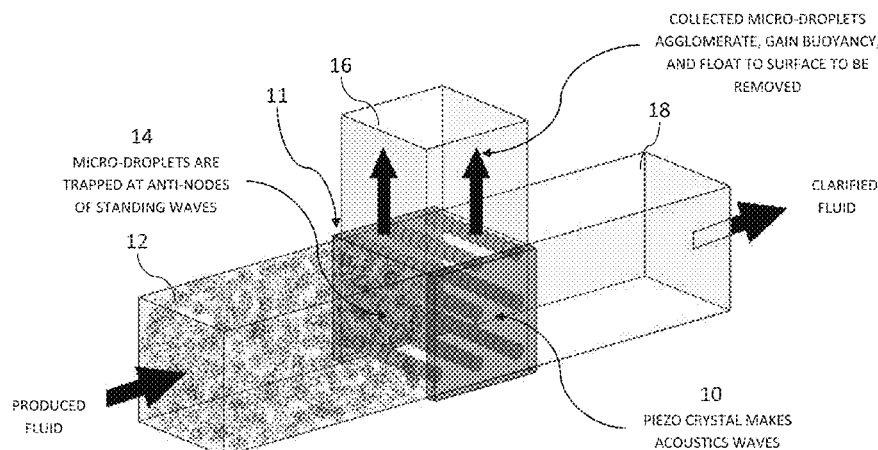
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(57) **ABSTRACT**

An apparatus for separating particles from a fluid stream includes a flow chamber that has at least one inlet and at least one outlet. At least one ultrasonic transducer is located on a wall of the flow chamber. The transducer includes a piezoelectric array with at least two piezoelectric elements. The piezoelectric array includes a piezoelectric material to create a multi-dimensional acoustic standing wave in the flow chamber. A reflector is located on the wall on the opposite side of the flow chamber from the at least one ultrasonic transducer.

22 Claims, 22 Drawing Sheets



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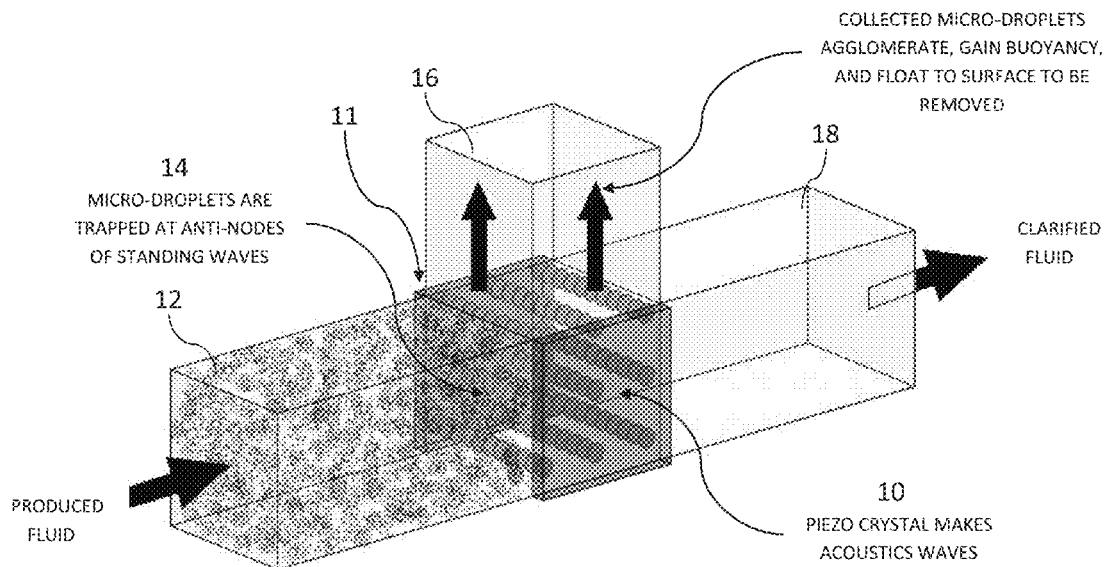


FIGURE 1A

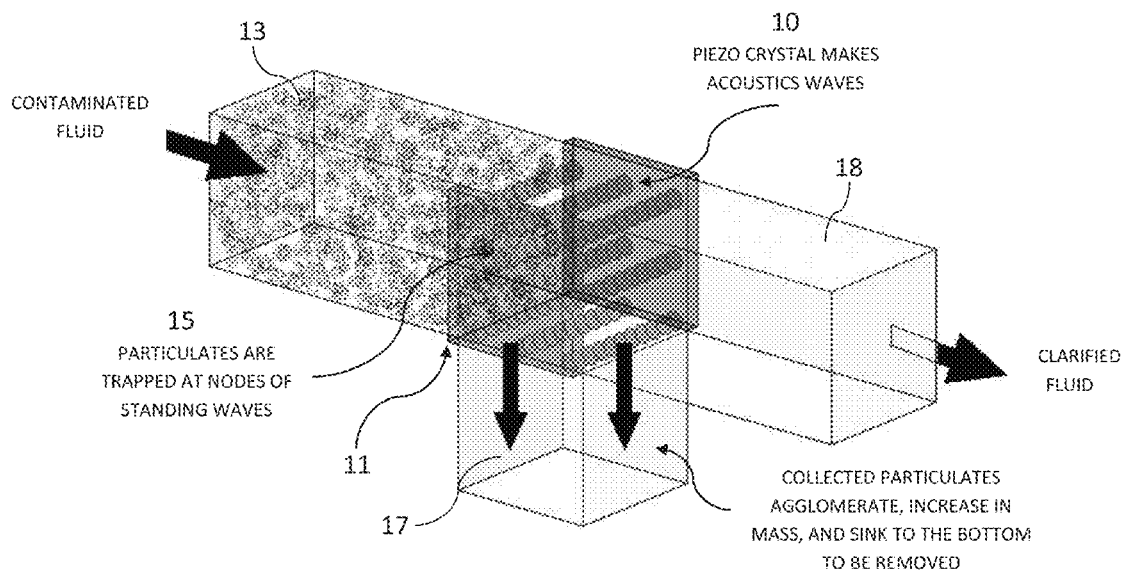


FIGURE 1B

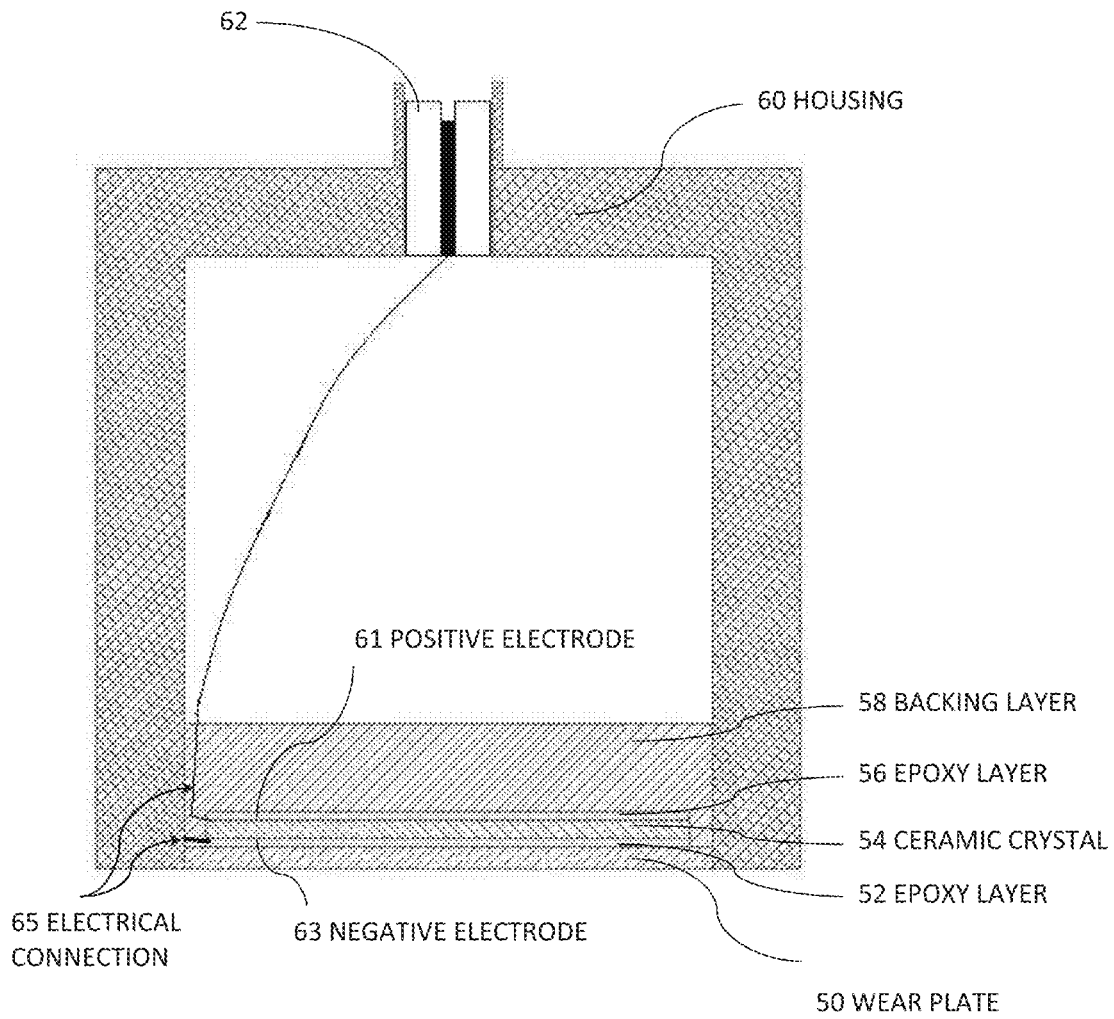


FIGURE 2

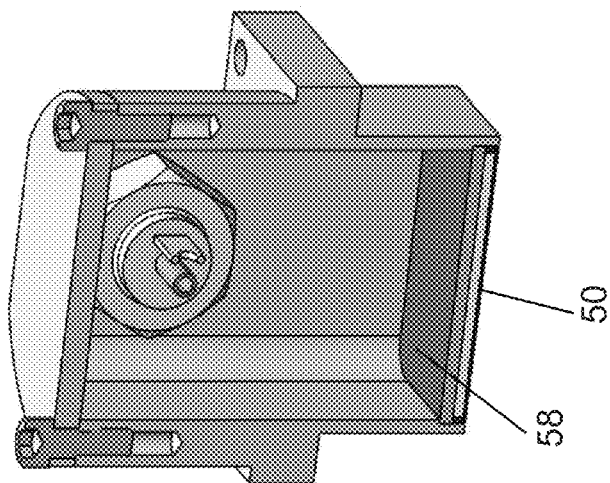


FIGURE 3B

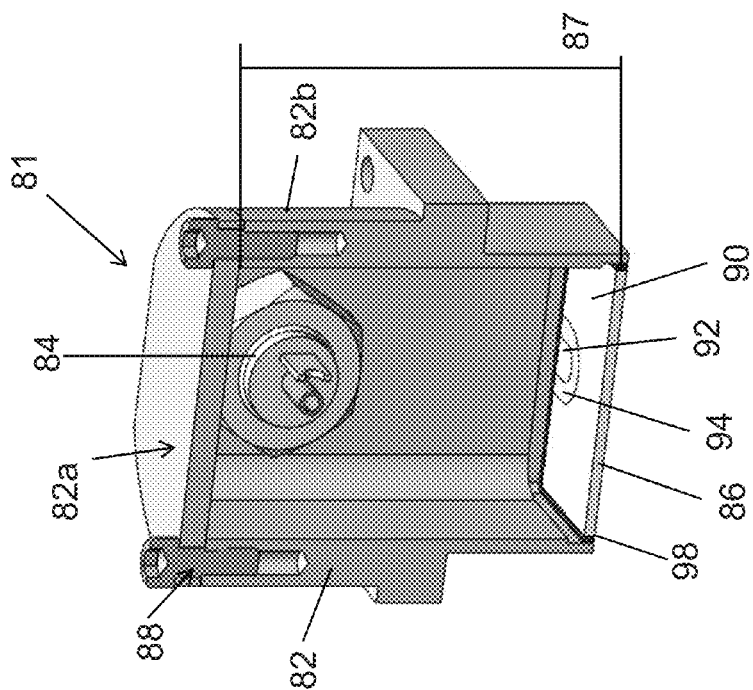


FIGURE 3A

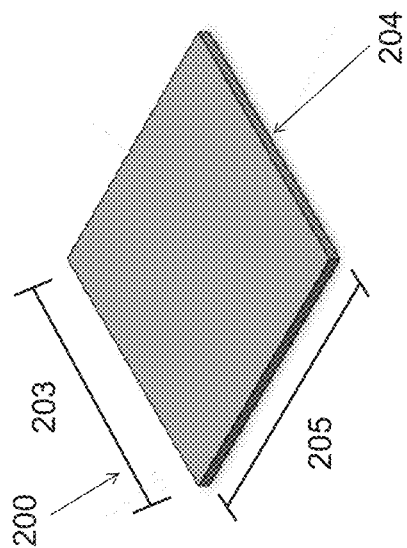


FIGURE 4

200''

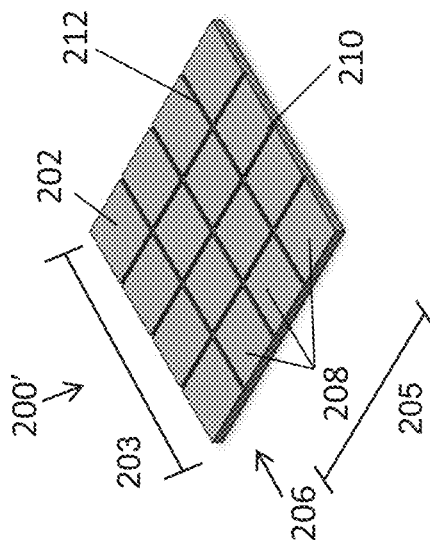


FIGURE 5

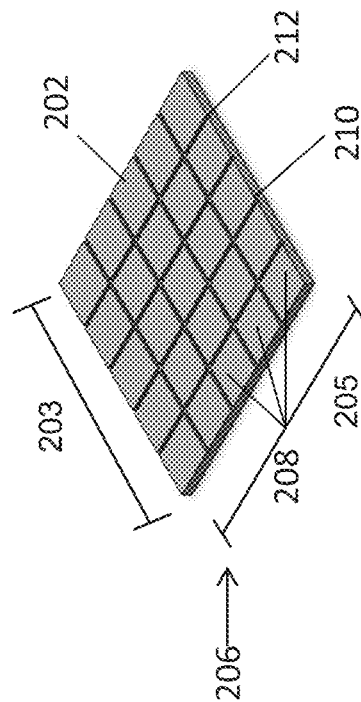


FIGURE 6

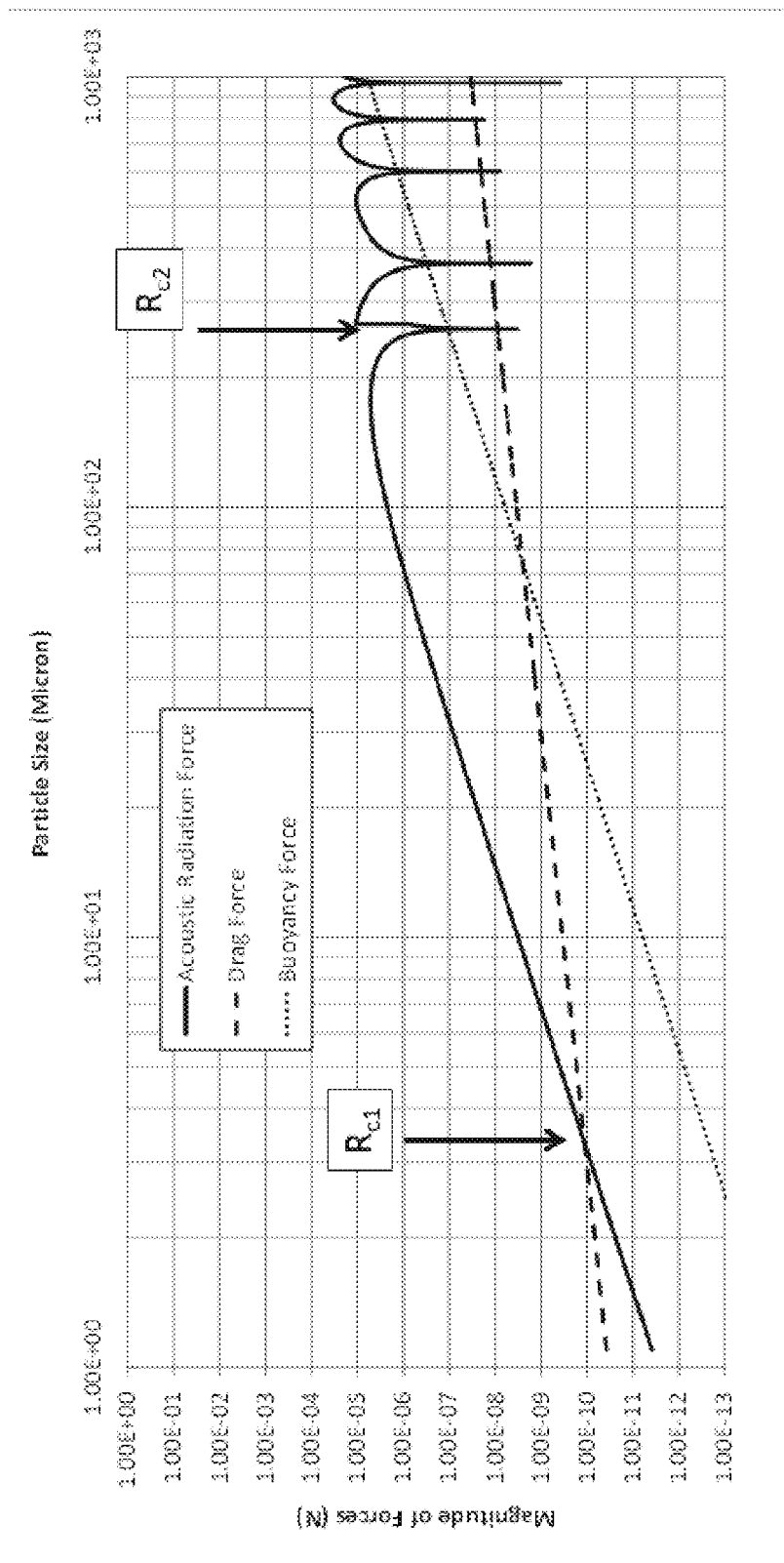


FIGURE 7

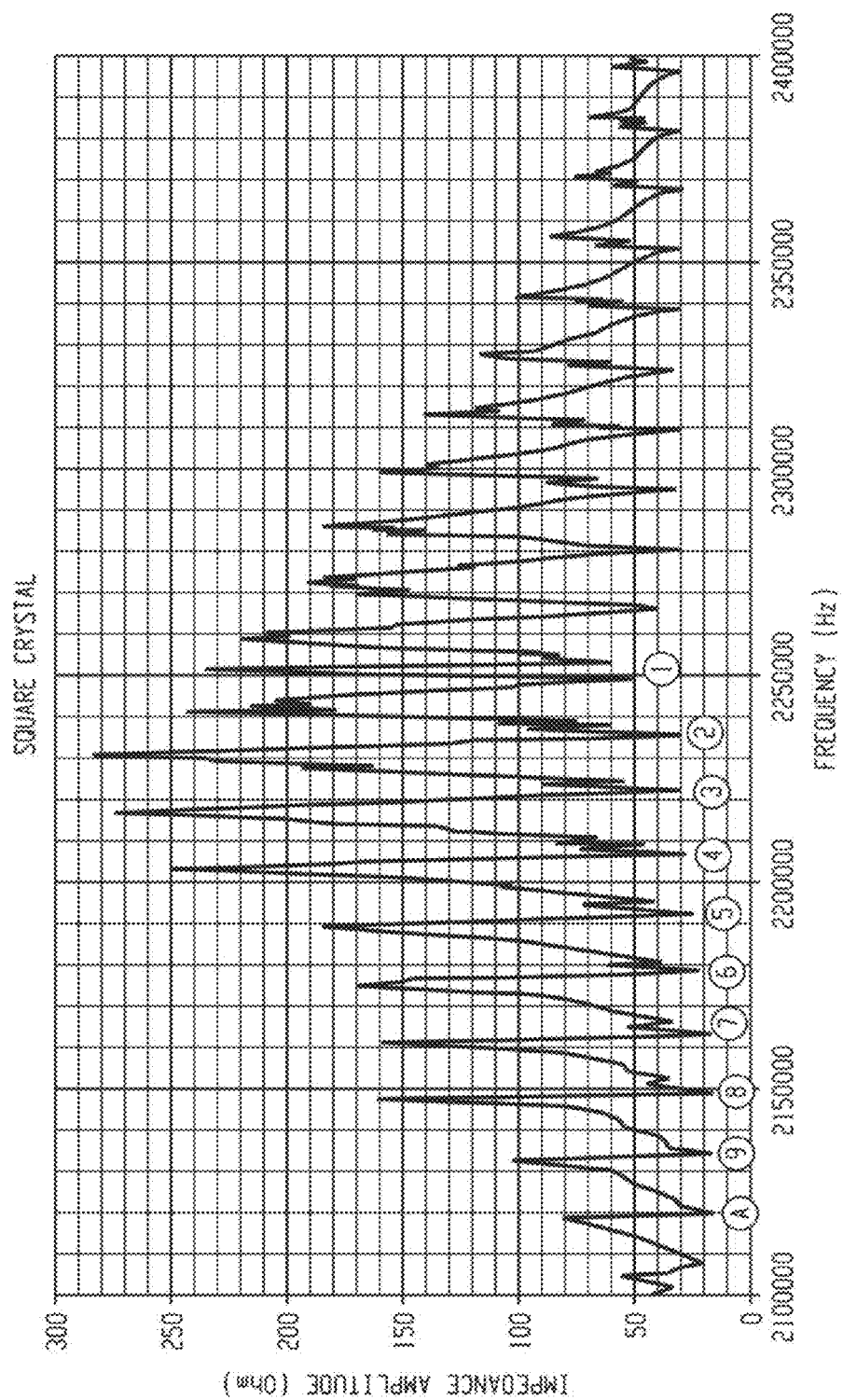


FIGURE 8

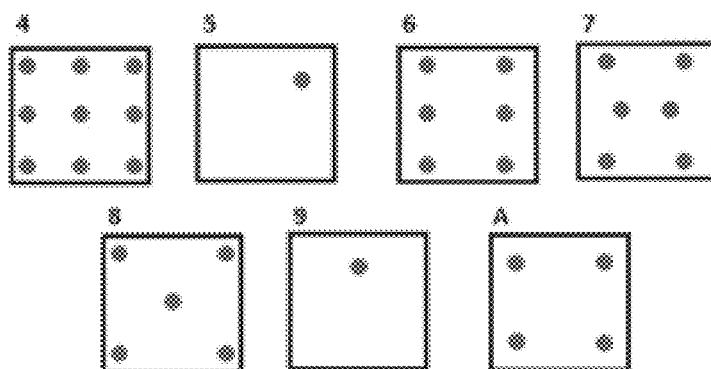


FIGURE 9A

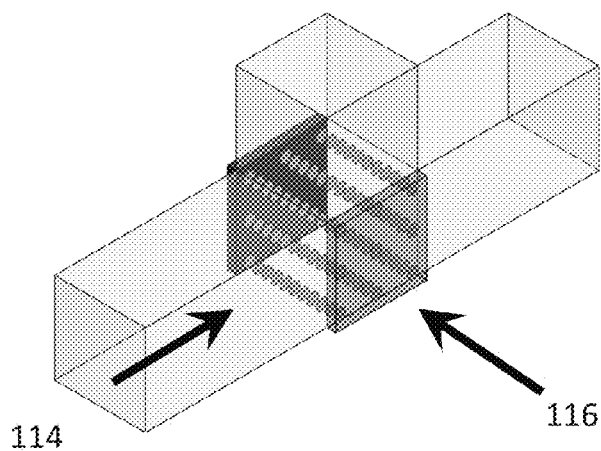


FIGURE 9B

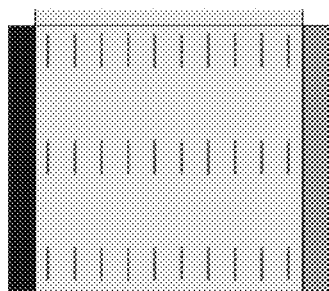


FIGURE 9C

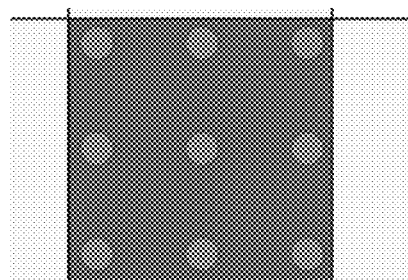


FIGURE 9D

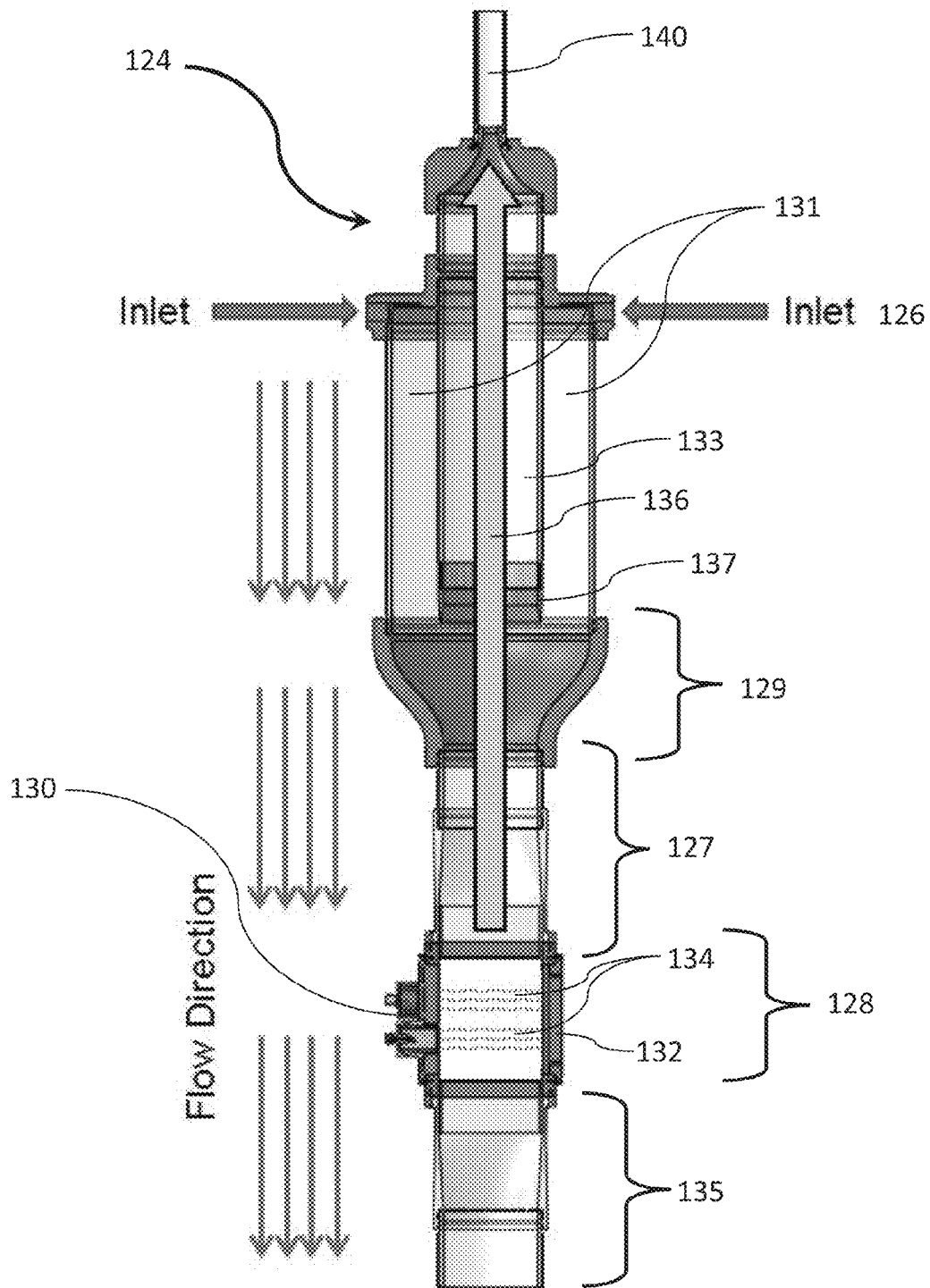


FIGURE 10A

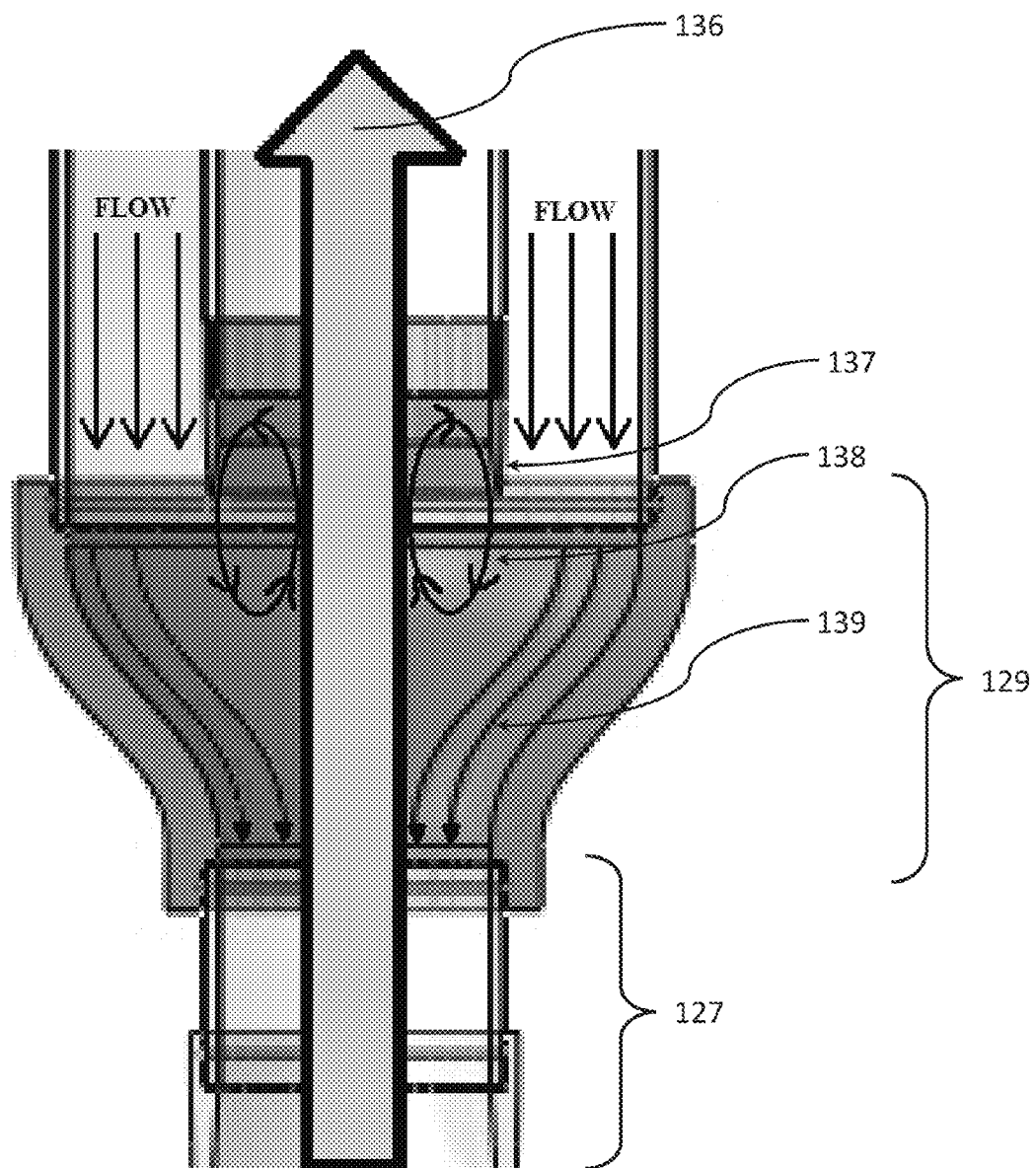


FIGURE 10B

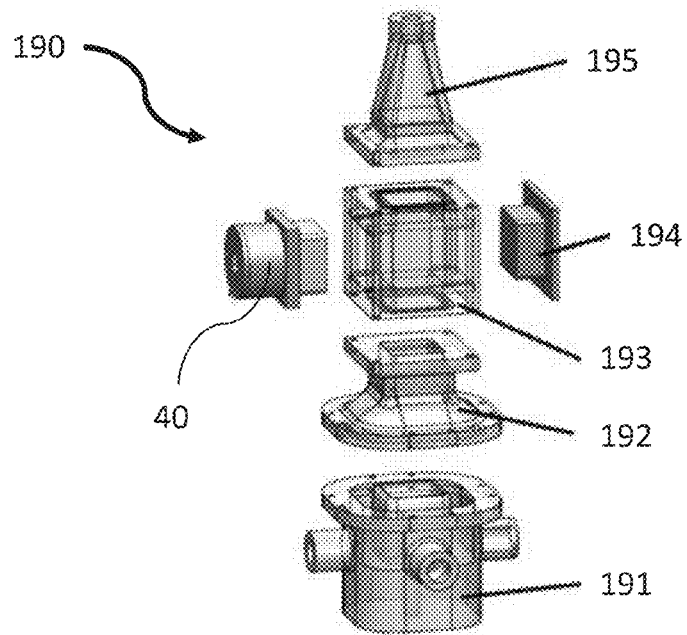


FIGURE 11A

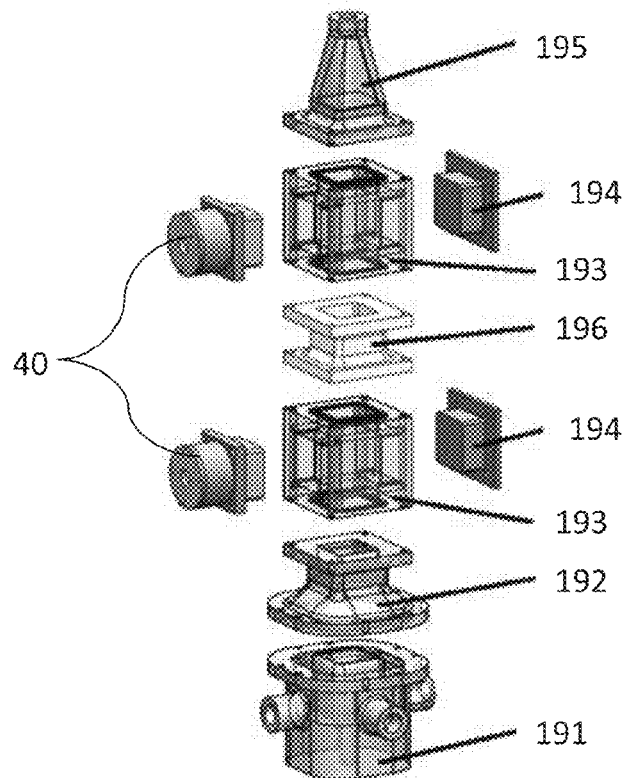


FIGURE 11B

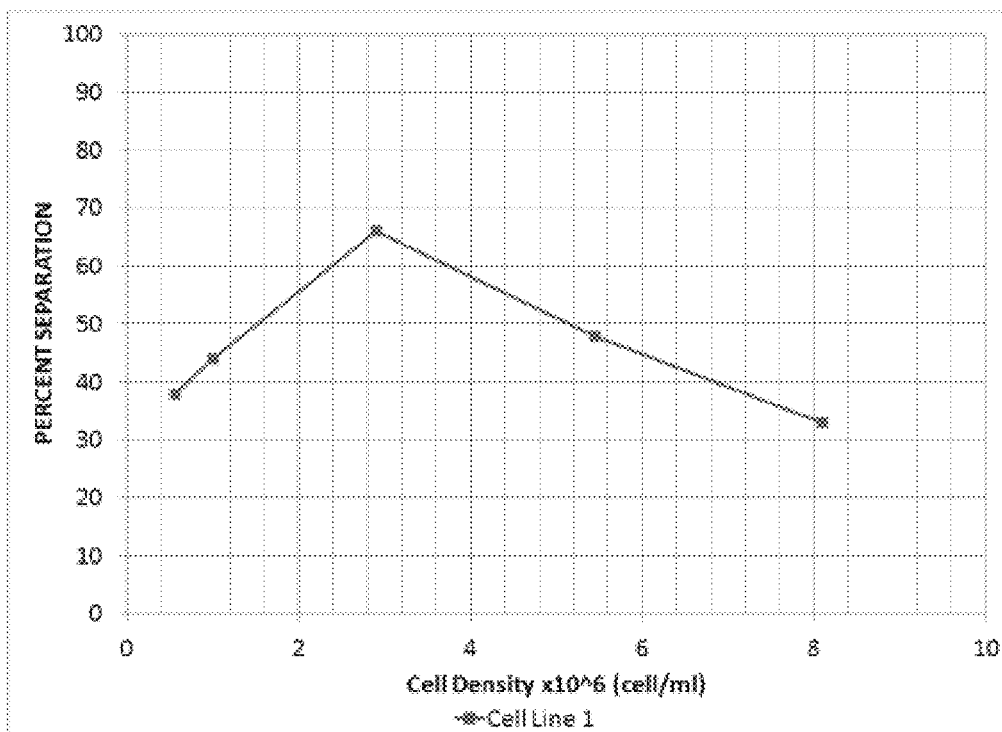


FIGURE 12A

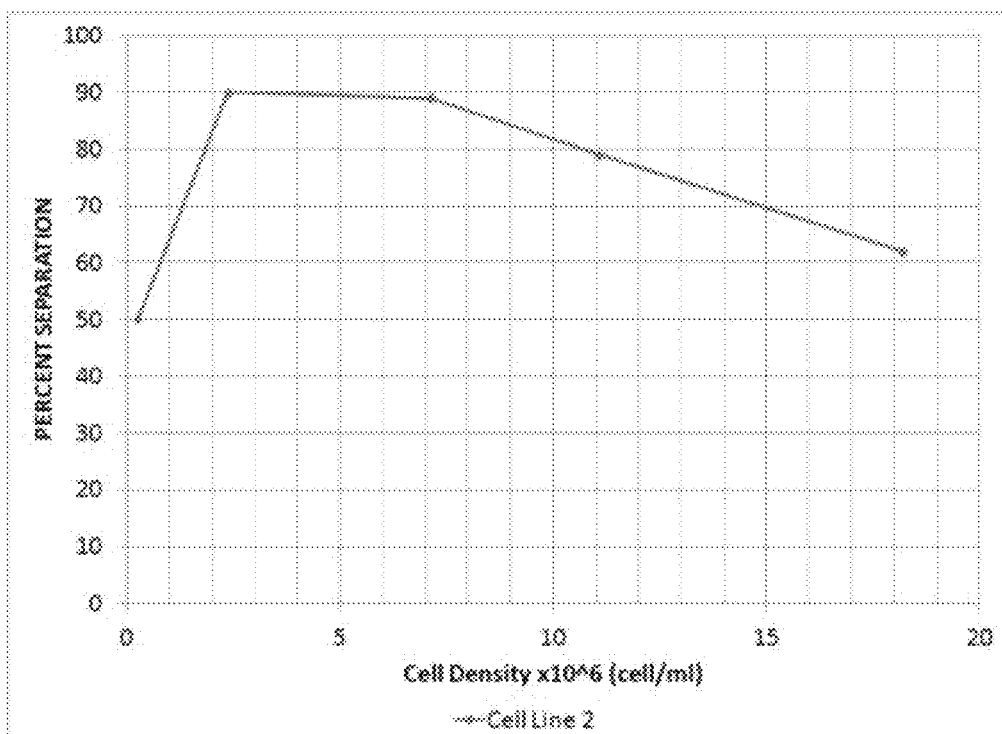


FIGURE 12B

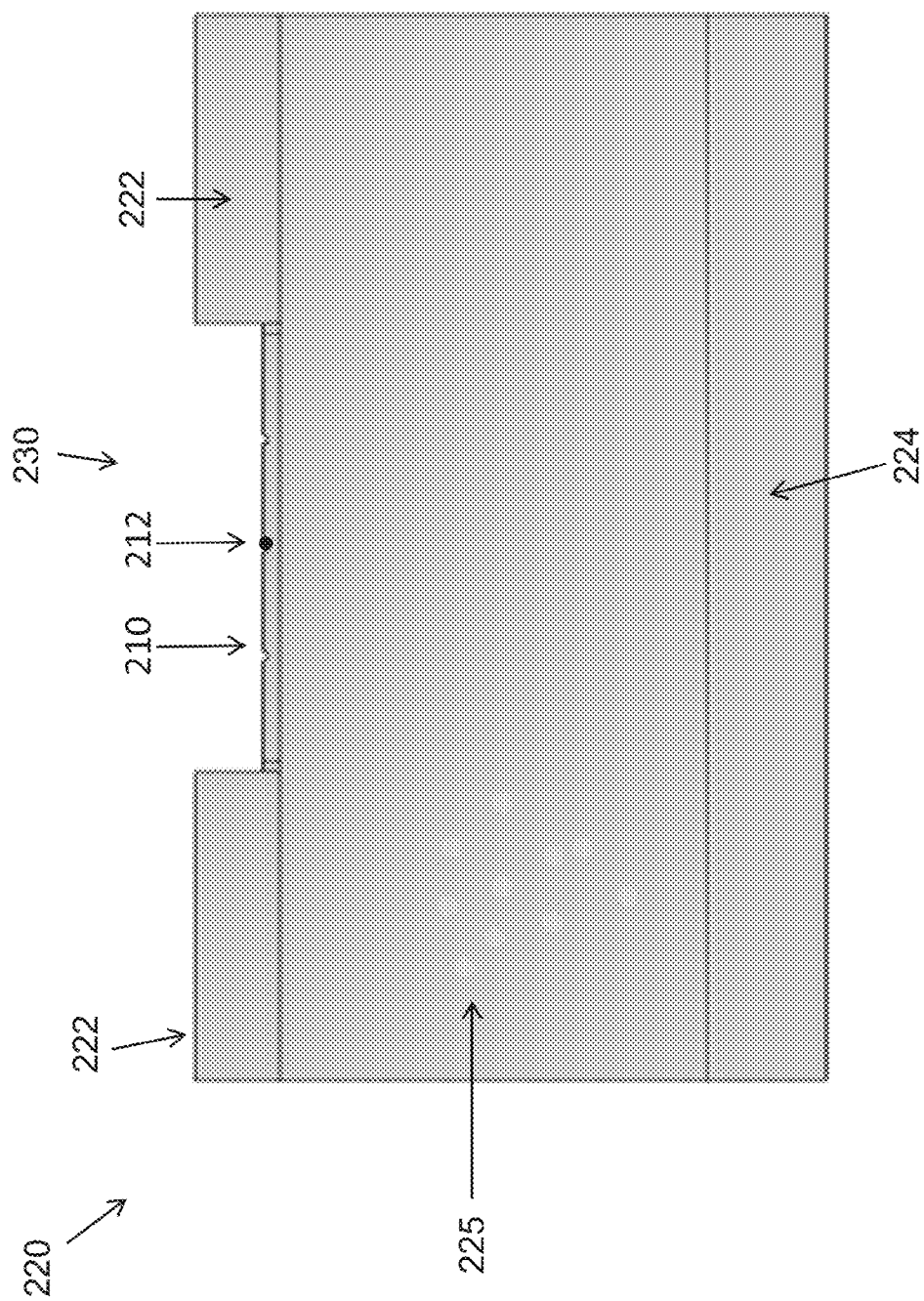
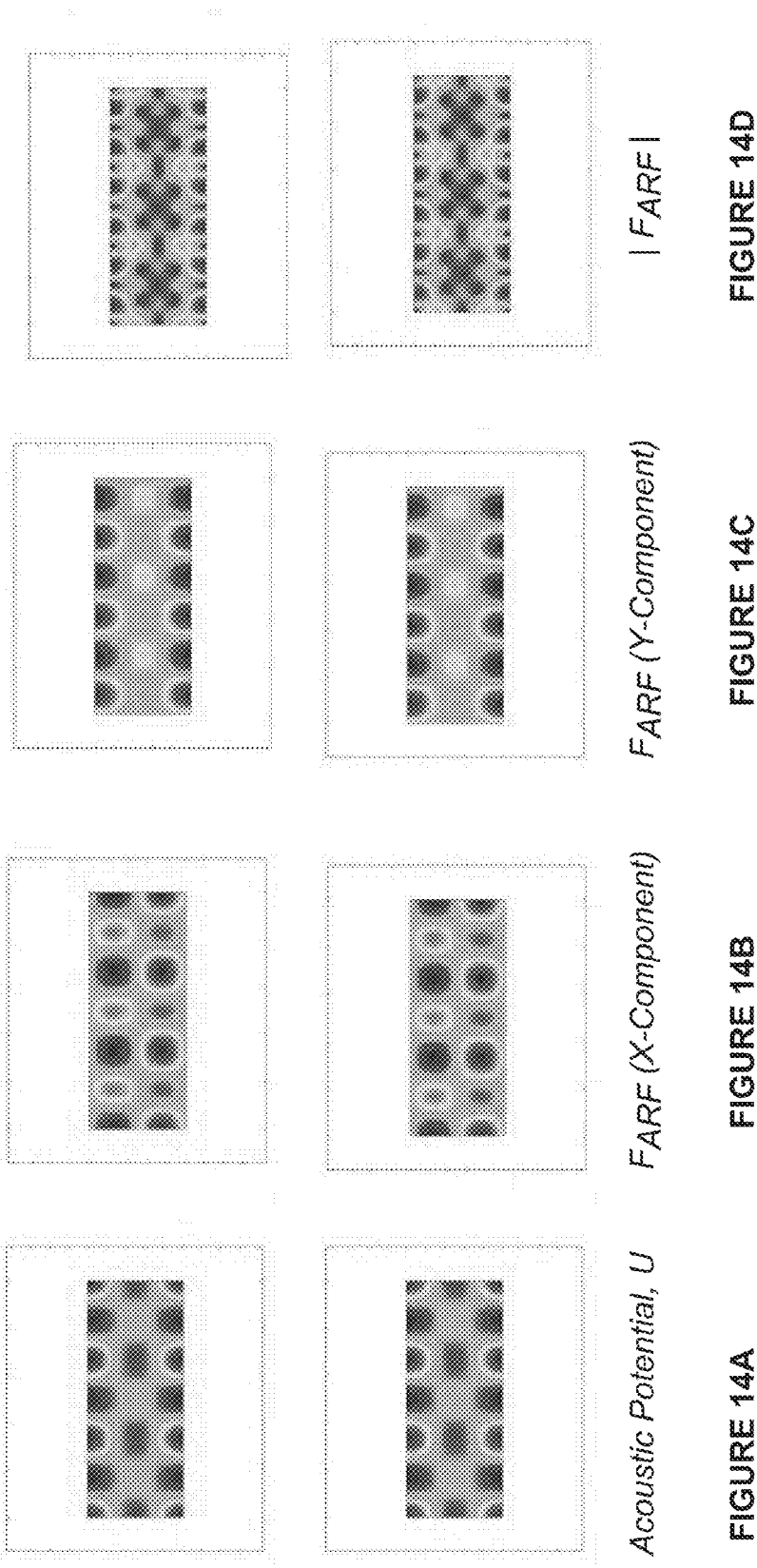


FIGURE 13



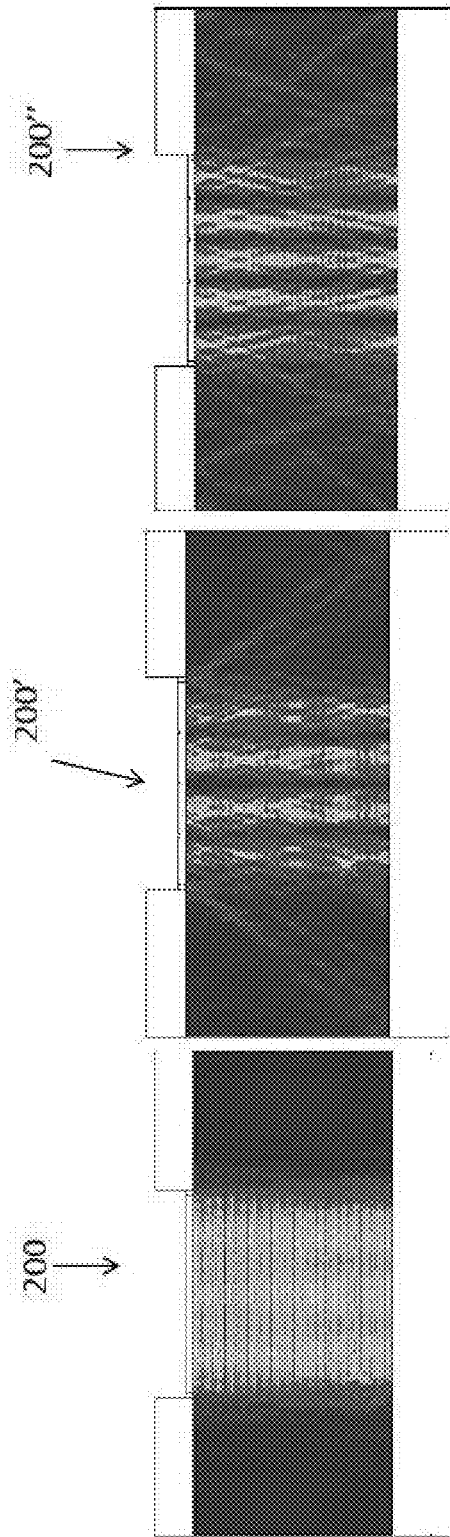


FIGURE 15

FIGURE 16

FIGURE 17

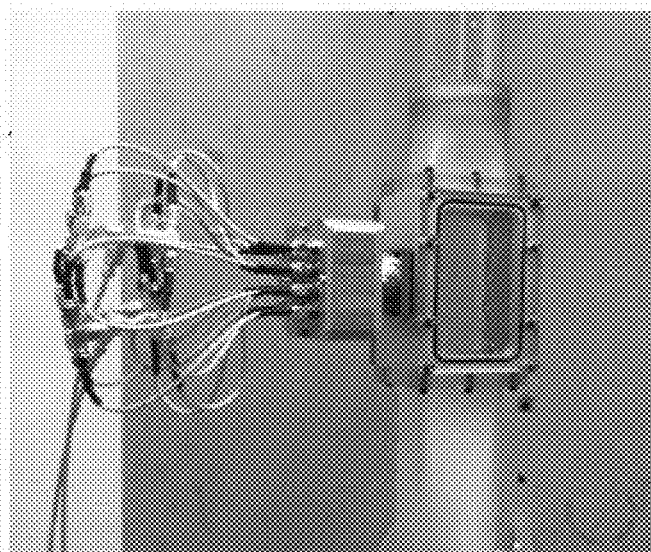


FIGURE 18

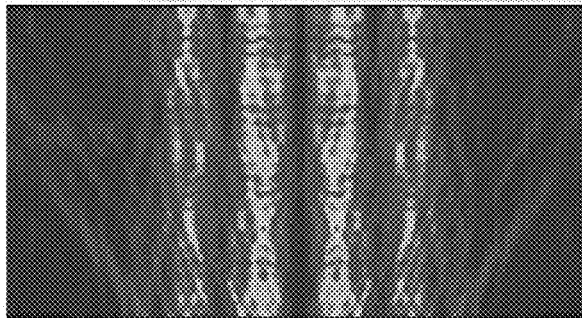
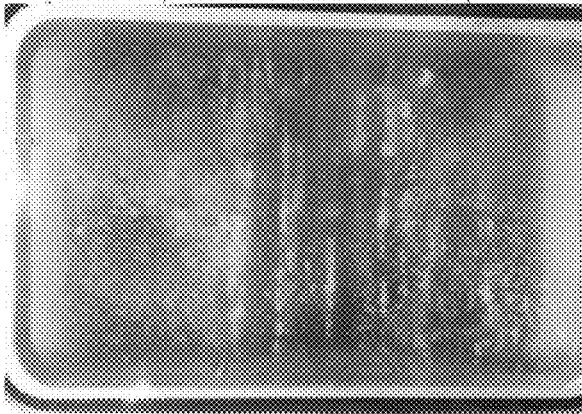
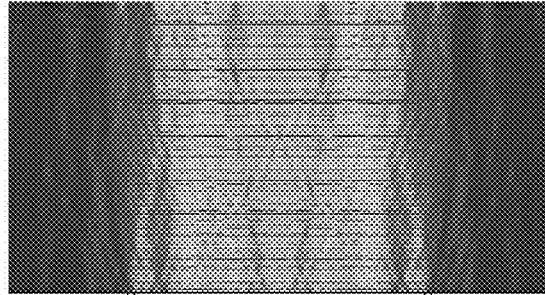
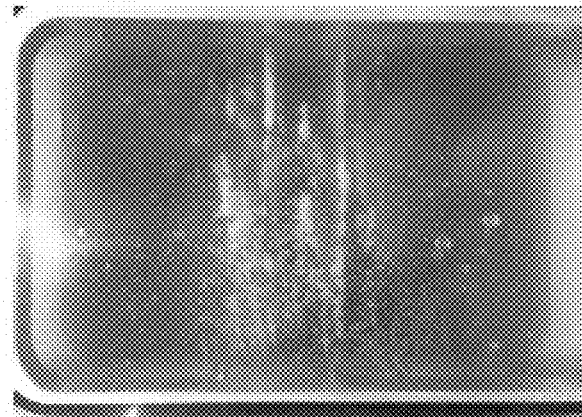


FIGURE 20

FIGURE 19

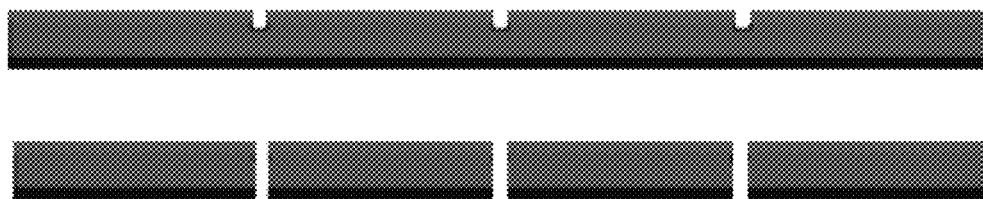


FIGURE 21



FIGURE 22

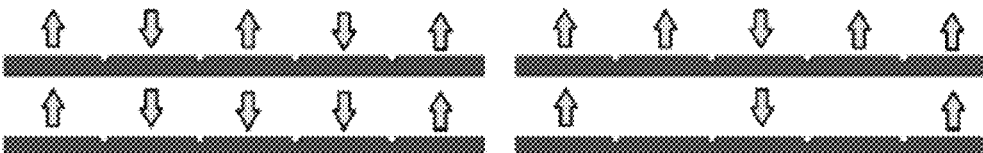


FIGURE 23

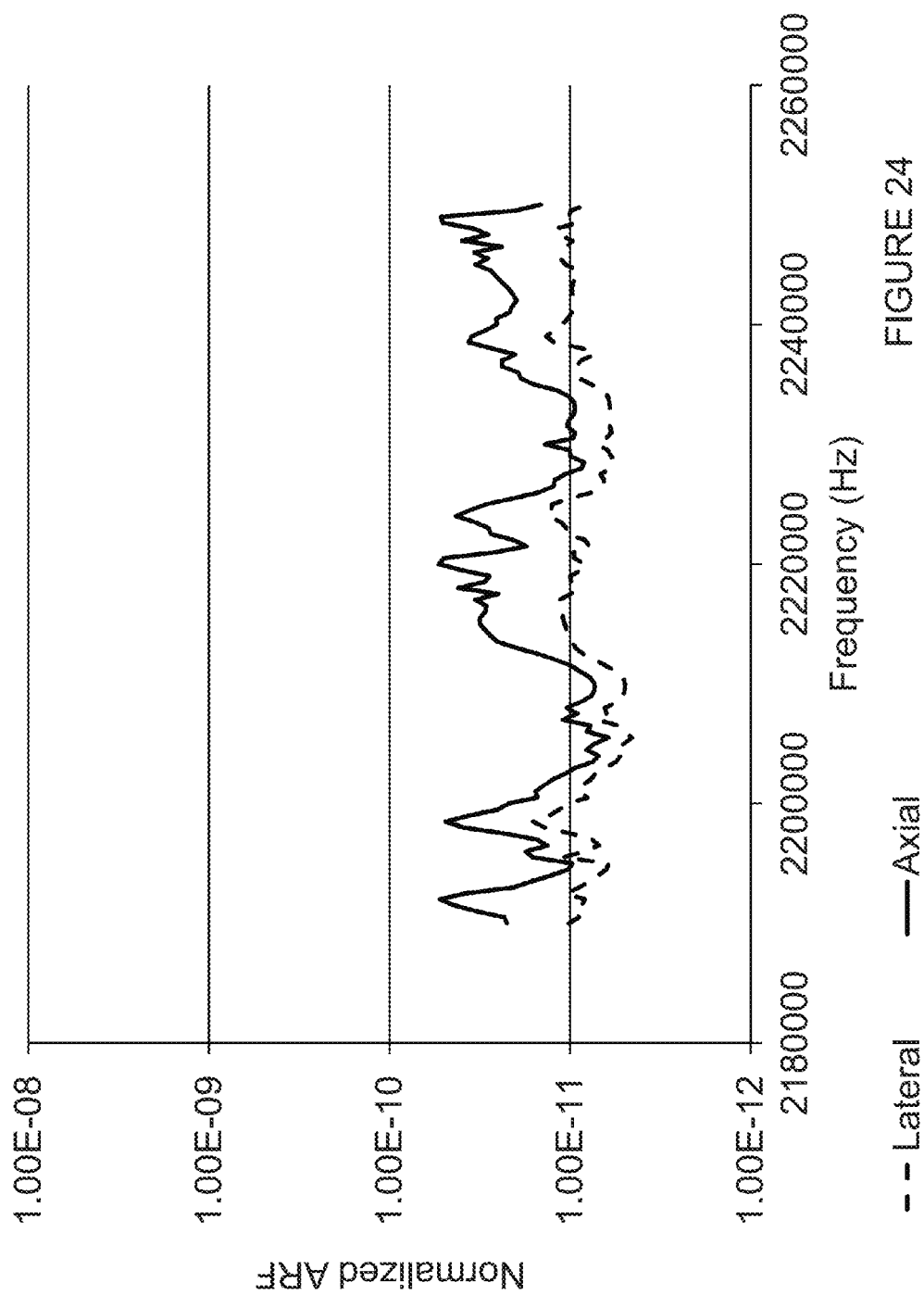
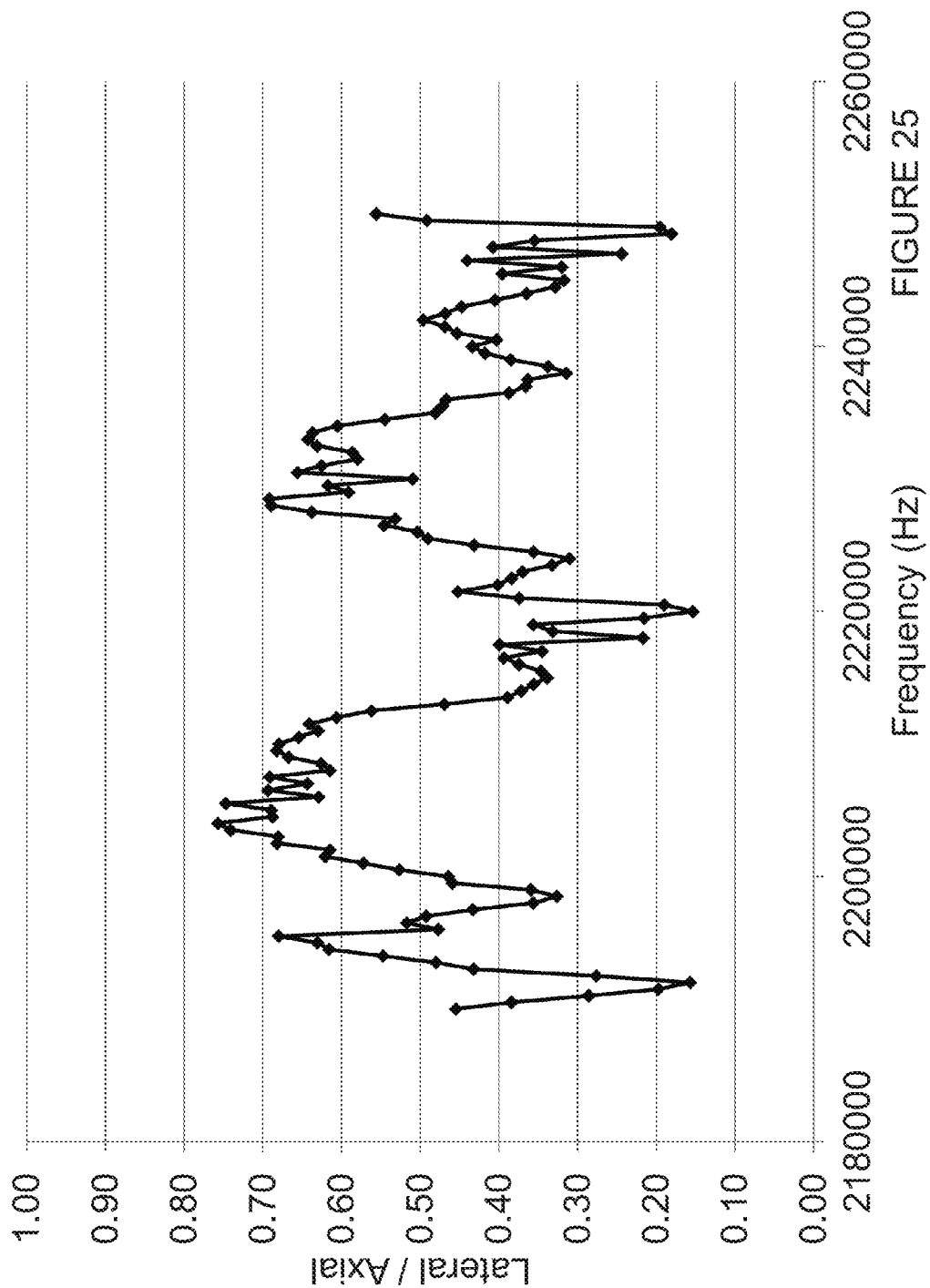


FIGURE 24



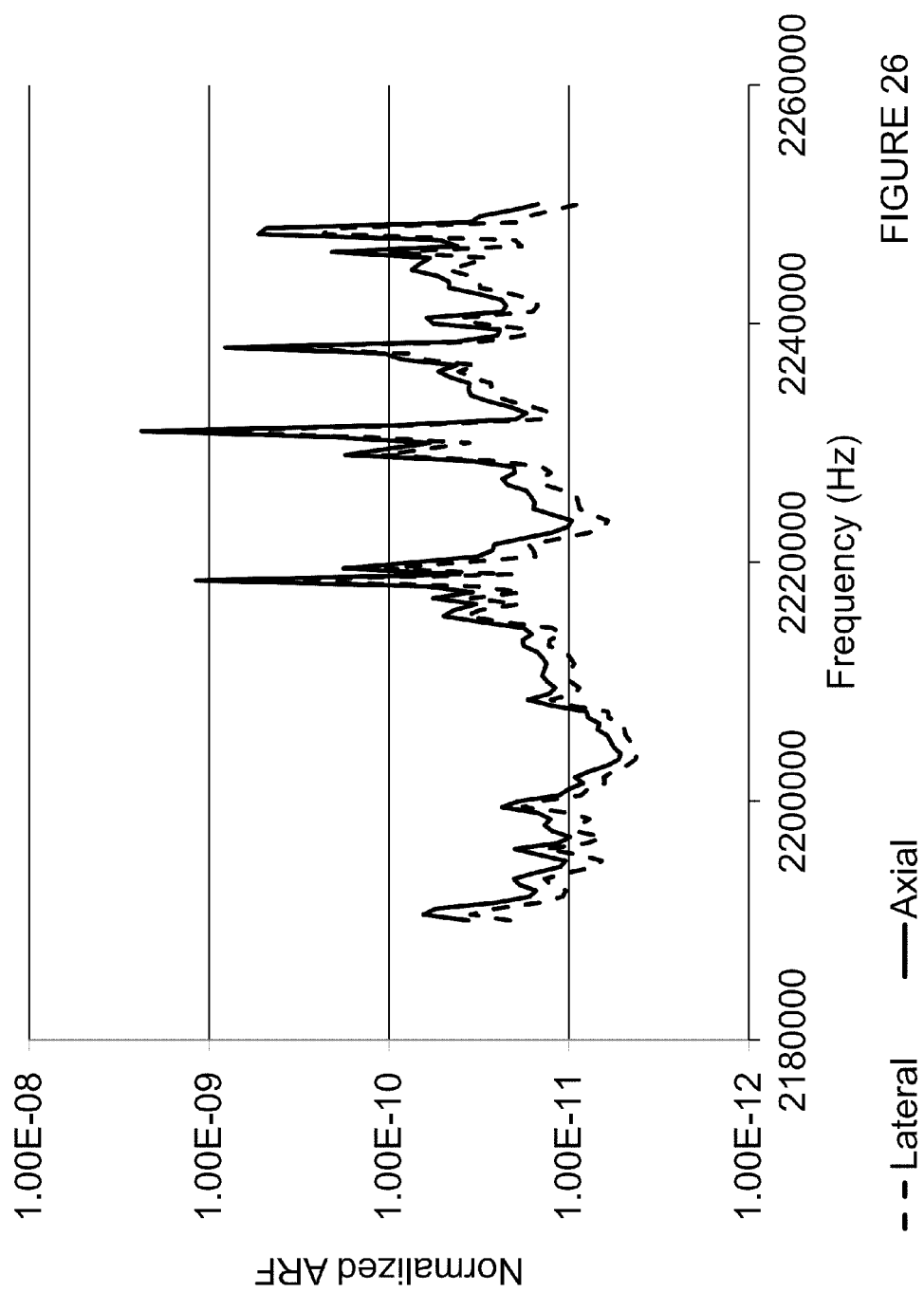


FIGURE 26

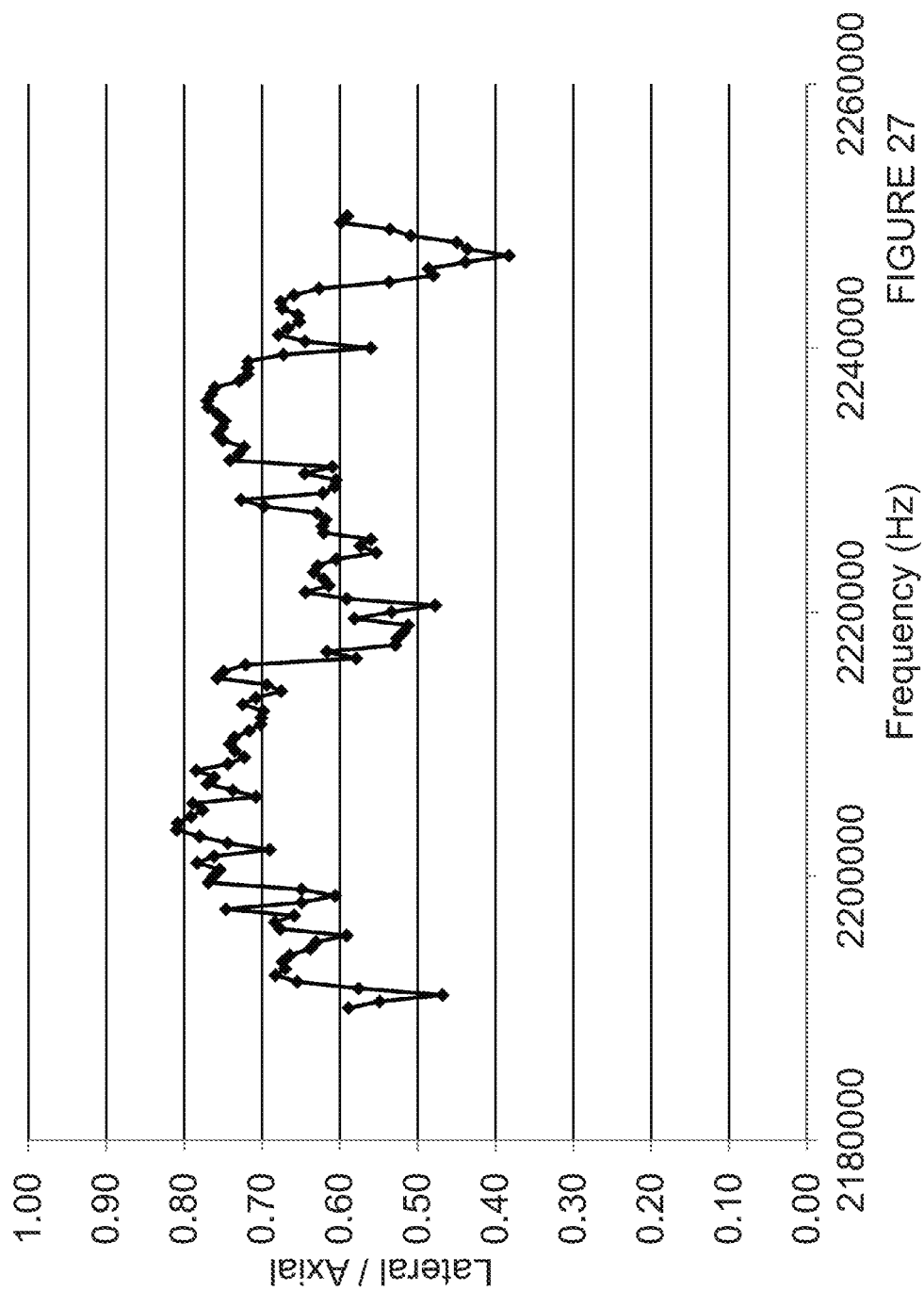


FIGURE 27

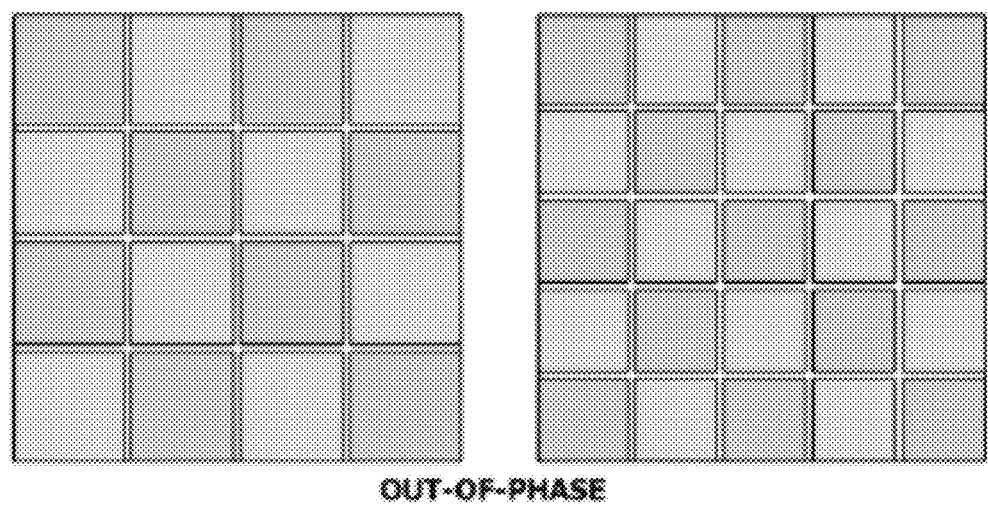


FIGURE 28

ACOUSTOPHORETIC DEVICE WITH PIEZOELECTRIC TRANSDUCER ARRAY

This application is a continuation-in-part of U.S. patent application Ser. No. 14/026,413, filed Sep. 13, 2013, which is a continuation-in-part of U.S. patent application Ser. No. 13/844,754, filed Mar. 15, 2013, which claimed the benefit of U.S. Provisional Patent Application Ser. No. 61/611,159, filed Mar. 15, 2012, and of U.S. Provisional Patent Application Ser. No. 61/611,240, also filed Mar. 15, 2012, and of U.S. Provisional Patent Application Ser. No. 61/754,792, filed Jan. 21, 2013. These applications are incorporated herein by reference in their entireties.

BACKGROUND

The ability to separate a particle/fluid mixture into its separate components is desirable in many applications. Acoustophoresis is the separation of particles using high intensity sound waves, and without the use of membranes or physical size exclusion filters. It has been known that high intensity standing waves of sound can exert forces on particles in a fluid when there is a differential in both density and/or compressibility, otherwise known as the acoustic contrast factor. The pressure profile in a standing wave contains areas of local minimum pressure amplitudes at its nodes and local maxima at its anti-nodes. Depending on the density and compressibility of the particles, they will be trapped at the nodes or anti-nodes of the standing wave. The higher the frequency of the standing wave, the smaller the particles that can be trapped due the pressure of the standing wave.

Efficient separation technologies for multi-component liquid streams that eliminate any waste and reduce the required energy, thereby promoting a sustainable environment, are needed.

BRIEF DESCRIPTION

The present disclosure relates to systems and devices for acoustophoresis on preferably a large scale. The devices use one or more unique ultrasonic transducers as described herein. The transducer includes a rectangular array made from a plurality of piezoelectric elements. The transducer is driven at frequencies that produce multi-dimensional standing waves.

Disclosed in various embodiments herein are apparatuses for separating a second fluid or a particulate from a host fluid, comprising: a flow chamber having at least one inlet and at least one outlet; at least one ultrasonic transducer located on a wall of the flow chamber, the transducer including a piezoelectric array formed from a plurality of piezoelectric elements which can be driven by a voltage signal to create a multi-dimensional acoustic standing wave in the flow chamber; and at least one reflector located on the wall on the opposite side of the flow chamber from the at least one ultrasonic transducer. The axial and lateral acoustic forces are of the same order of magnitude. The second fluid or particulate agglomerates at the pressure nodes (minima of the acoustic radiation potential) of the multi-dimensional acoustic standing wave, and continuously falls out of the multi-dimensional acoustic standing wave due to gravity separation, or continuously rises out of the multi-dimensional acoustic standing wave due to buoyancy.

In some embodiments, the piezoelectric array is present on a single crystal, with one or more channels separating the piezoelectric elements from each other. A potting material

different from the piezoelectric material can be present in the one or more channels. The potting material may be a polymer, such as an epoxy.

In other embodiments, each piezoelectric element is physically separated from surrounding piezoelectric elements by a potting material. The potting material may be a polymer, such as an epoxy.

The piezoelectric array can be a rectangular array. Each piezoelectric element may have the same dimensions. Each piezoelectric element may be individually connected to its own pair of electrodes.

In particular embodiments, a contoured nozzle wall is located upstream of the at least one inlet of the flow chamber.

Also disclosed are methods of separating a second fluid or a particulate from a host fluid, comprising: flowing a mixture of the host fluid and the second fluid or particulate through an apparatus, the apparatus comprising: a flow chamber having at least one inlet and at least one outlet; at least one ultrasonic transducer located on a wall of the flow chamber, the transducer including a piezoelectric array formed from a plurality of piezoelectric elements which can be driven by a voltage signal to create a multi-dimensional standing wave in the flow chamber; and at least one reflector located on the wall on the opposite side of the flow chamber from the at least one ultrasonic transducer; and sending voltage signals to the piezoelectric array to form a multi-dimensional acoustic standing wave that traps the second fluid or particulate against the flow of the fluid, permitting agglomeration such that the second fluid or particulate increases in size and continuously falls out of the multi-dimensional acoustic standing wave through gravity separation. The separated material may be swept from the chamber by the fluid flow, collected in a pocket, or compacted into a smaller volume.

The particulate may be Chinese hamster ovary (CHO) cells, NS0 hybridoma cells, baby hamster kidney (BHK) cells, or human cells.

Sometimes, the piezoelectric elements are operated out of phase with each other. Other times, the piezoelectric elements are operated in phase with each other.

The flow rate of the host fluid through the flow chamber may be at least 25 mL/min. The piezoelectric elements may be operated at a frequency in a range of 100 kHz to 20 MHz, or in more specific embodiments from about 2 MHz to about 2.5 MHz.

In most embodiments, the multi-dimensional standing wave results in an acoustic radiation force having an axial force component and a lateral force component that are of the same order of magnitude.

The piezoelectric array can be present on a single crystal, with one or more channels separating the piezoelectric elements from each other. A potting material different from the piezoelectric material may be present in the one or more channels.

In other embodiments, each piezoelectric element is physically separated from surrounding piezoelectric elements by a potting material. Each piezoelectric element may be individually connected to its own pair of electrodes.

These and other non-limiting characteristics are more particularly described below.

BRIEF DESCRIPTION OF THE DRAWINGS

The following is a brief description of the drawings, which are presented for the purposes of illustrating the exemplary embodiments disclosed herein and not for the purposes of limiting the same.

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FIG. 1A is a diagram illustrating the function of an acoustophoretic separator with a secondary fluid or particles less dense than the host fluid.

FIG. 1B is a diagram illustrating the function of an acoustophoretic separator with a secondary fluid or particles denser than the host fluid.

FIG. 2 is a cross-sectional diagram of a conventional ultrasonic transducer.

FIG. 3A is a cross-sectional diagram of an ultrasonic transducer structure that can be used in the present disclosure. An air gap is present within the transducer, and no backing layer or wear plate is present.

FIG. 3B is a cross-sectional diagram of an ultrasonic transducer structure that can be used in the present disclosure. An air gap is present within the transducer, and a backing layer and wear plate are present.

FIG. 4 is a conventional single-piece monolithic piezoelectric crystal used in an ultrasonic transducer.

FIG. 5 is an exemplary rectangular piezoelectric array having 16 piezoelectric elements used in the transducers of the present disclosure.

FIG. 6 is another exemplary rectangular piezoelectric array having 25 piezoelectric elements used in the transducers of the present disclosure.

FIG. 7 is a graph showing the relationship of the acoustic radiation force, gravity/buoyancy force, and Stokes' drag force to particle size. The horizontal axis is in microns (μm) and the vertical axis is in Newtons (N).

FIG. 8 is a graph of electrical impedance amplitude versus frequency for a square transducer driven at different frequencies.

FIG. 9A illustrates the trapping line configurations for seven of the minima amplitudes of FIG. 8 from the direction orthogonal to fluid flow.

FIG. 9B is a perspective view illustrating the separator. The fluid flow direction and the trapping lines are shown.

FIG. 9C is a view from the fluid inlet along the fluid flow direction (arrow 114) of FIG. 9B, showing the trapping nodes of the standing wave where particles would be captured.

FIG. 9D is a view taken through the transducers face at the trapping line configurations, along arrow 116 as shown in FIG. 9B.

FIG. 10A shows an acoustophoretic separator for separating buoyant materials.

FIG. 10B is a magnified view of fluid flow near the intersection of the contoured nozzle wall 129 and the collection duct 137.

FIG. 11A shows an exploded view of an acoustophoretic separator used in Bio-Pharma applications.

FIG. 11B shows an exploded view of a stacked acoustophoretic separator with two acoustic chambers.

FIG. 12A is a graph showing the efficiency of removing cells from a medium using a Beckman Coulter Cell Viability Analyzer for one experiment.

FIG. 12B is a graph showing the efficiency of removing cells from a medium using a Beckman Coulter Cell Viability Analyzer for another experiment.

FIG. 13 shows a schematic of a two-dimensional numerical model developed for the simulation of an ultrasonic transducer and transducer array.

FIGS. 14A-14D are diagrams comparing the results of the numerical model (bottom) of FIG. 13 against published data (top), illustrating the accuracy of the numerical model. FIG. 14A compares the acoustic potential U. FIG. 14B compares the x-component of the acoustic radiation force (ARF). FIG.

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14C compares the y-component of the ARF. FIG. 14D compares the absolute value of the ARF.

FIG. 15 is a diagram showing the amplitude of the acoustic standing wave generated by a monolithic piezoelectric crystal in the model of FIG. 13. The frequency is at 2.245 MHz. The horizontal axis is the location along the X-axis, and the vertical axis is the location along the Y-axis between the transducer and the reflector.

FIG. 16 is a diagram showing the amplitude of the acoustic standing wave generated by the 4-element piezoelectric array in the model of FIG. 13. The frequency is at 2.245 MHz with phasing between the elements being varied.

FIG. 17 is a diagram showing the amplitude of the acoustic standing wave generated by the 5-element piezoelectric array in the model of FIG. 13. The frequency is at 2.245 MHz with phasing between the elements being varied.

FIG. 18 is a picture of an acoustophoretic setup with a 4x4 piezoelectric array made from a 2 MHz PZT-8 crystal with kerfs made in the crystal, as shown in FIG. 5.

FIG. 19 is a comparison of the simulation of an out-of-phase piezoelectric array with an actual acoustophoretic experiment using the out-of-phase array. For this simulation, out-of-phase refers to the phase angle of the delivered voltage. For out-of-phase testing, the phasing varied from 0° - 180° - 0° - 180° for the numerical model. For the experimental test, the elements were varied in a checkerboard pattern.

FIG. 20 is a comparison of the simulation of an in-phase piezoelectric array with an actual acoustophoretic experiment using the in-phase array. For this simulation, in-phase refers to the phase angle of the delivered voltage. For in-phase testing, the phasing was kept constant between all elements.

FIG. 21 is a picture illustrating a kerfed crystal (top) versus a transducer array that has piezoelectric elements joined together by a potting material (bottom).

FIG. 22 is a diagram showing the out-of-phase modes tested for the 4-element array.

FIG. 23 is a diagram showing the out-of-phase modes tested for the 5-element array.

FIG. 24 is a graph showing the normalized acoustic radiation force (ARF) from a monolithic piezoelectric crystal simulation.

FIG. 25 is a graph showing the ratio of the ARF components (lateral to axial) for a monolithic piezoelectric crystal simulation.

FIG. 26 is a graph showing the normalized acoustic radiation force (ARF) for a 5-element simulation with varying phasing.

FIG. 27 is a graph showing the ratio of the ARF components (lateral to axial) for the 5-element simulation.

FIG. 28 is a diagram showing the phasing of the arrays during out-of-phase testing. Dark elements had a 0° phase angle and light element had a 180° phase angle when tested

DETAILED DESCRIPTION

The present disclosure may be understood more readily by reference to the following detailed description of desired embodiments and the examples included therein. In the following specification and the claims which follow, reference will be made to a number of terms which shall be defined to have the following meanings.

The singular forms "a," "an," and "the" include plural referents unless the context clearly dictates otherwise.

The term "comprising" is used herein as requiring the presence of the named components/steps and allowing the

presence of other components/steps. The term “comprising” should be construed to include the term “consisting of”, which allows the presence of only the named components/steps, along with any impurities that might result from the manufacture of the named components/steps.

Numerical values should be understood to include numerical values which are the same when reduced to the same number of significant figures and numerical values which differ from the stated value by less than the experimental error of conventional measurement technique of the type described in the present application to determine the value.

All ranges disclosed herein are inclusive of the recited endpoint and independently combinable (for example, the range of “from 2 grams to 10 grams” is inclusive of the endpoints, 2 grams and 10 grams, and all the intermediate values).

The terms “substantially” and “about” can be used to include any numerical value that can vary without changing the basic function of that value. When used with a range, “substantially” and “about” also disclose the range defined by the absolute values of the two endpoints, e.g. “about 2 to about 4” also discloses the range “from 2 to 4.” The terms “substantially” and “about” may refer to plus or minus 10% of the indicated number.

It should be noted that many of the terms used herein are relative terms. For example, the terms “upper” and “lower” are relative to each other in location, i.e. an upper component is located at a higher elevation than a lower component in a given orientation, but these terms can change if the device is flipped. The terms “inlet” and “outlet” are relative to a fluid flowing through them with respect to a given structure, e.g. a fluid flows through the inlet into the structure and flows through the outlet out of the structure. The terms “upstream” and “downstream” are relative to the direction in which a fluid flows through various components, i.e. the flow fluids through an upstream component prior to flowing through the downstream component. It should be noted that in a loop, a first component can be described as being both upstream of and downstream of a second component.

The terms “horizontal” and “vertical” are used to indicate direction relative to an absolute reference, i.e. ground level. The terms “above” and “below”, or “upwards” and “downwards” are also relative to an absolute reference; an upwards flow is always against the gravity of the earth.

The present application refers to “the same order of magnitude.” Two numbers are of the same order of magnitude if the quotient of the larger number divided by the smaller number is a value less than 10.

The acoustophoretic separation technology of the present disclosure employs ultrasonic acoustic standing waves to trap, i.e., hold stationary, particles or a secondary fluid in a host fluid stream. The particles or secondary fluid collect at the nodes or anti-nodes of the multi-dimensional acoustic standing wave, depending on the particles’ or secondary fluid’s acoustic contrast factor relative to the host fluid, forming clusters that eventually fall out of the multi-dimensional acoustic standing wave when the clusters have grown to a size large enough to overcome the holding force of the multi-dimensional acoustic standing wave (e.g. by coalescence or agglomeration). This is an important distinction from previous approaches where particle trajectories were merely altered by the effect of the acoustic radiation force. The scattering of the acoustic field off the particles results in a three dimensional acoustic radiation force, which acts as a three-dimensional trapping field. The acoustic radiation

force is proportional to the particle volume (e.g. the cube of the radius) when the particle is small relative to the wavelength. It is proportional to frequency and the acoustic contrast factor. It also scales with acoustic energy (e.g. the square of the acoustic pressure amplitude). For harmonic excitation, the sinusoidal spatial variation of the force is what drives the particles to the stable axial positions within the standing waves. When the acoustic radiation force exerted on the particles is stronger than the combined effect of fluid drag force and buoyancy and gravitational force, the particle is trapped within the acoustic standing wave field. This results in concentration, agglomeration and/or coalescence of the trapped particles that will then continuously fall out of the multi-dimensional acoustic standing wave through gravity separation. The strong lateral forces create rapid clustering of particles. Relatively large solids of one material can thus be separated from smaller particles of a different material, the same material, and/or the host fluid through enhanced gravitational separation.

In this regard, the contrast factor is the difference between the compressibility and density of the particles and the fluid itself. These properties are characteristic of the particles and the fluid themselves. Most cell types present a higher density and lower compressibility than the medium in which they are suspended, so that the acoustic contrast factor between the cells and the medium has a positive value. As a result, the axial acoustic radiation force (ARF) drives the cells, with a positive contrast factor, to the pressure nodal planes, whereas cells or other particles with a negative contrast factor are driven to the pressure anti-nodal planes. The radial or lateral component of the acoustic radiation force trap the cells. The radial or lateral component of the ARF is larger than the combined effect of fluid drag force and gravitational force. The radial or lateral component drives the cells/particles to planes where they can cluster into larger groups, which will then gravity separate from the fluid.

As the cells agglomerate at the nodes of the standing wave, there is also a physical scrubbing of the cell culture media that occurs whereby more cells are trapped as they come in contact with the cells that are already held within the standing wave. This generally separates the cells from the cell culture media. The expressed biomolecules remain in the nutrient fluid stream (i.e. cell culture medium).

For three-dimensional acoustic fields, Gor’kov’s formulation can be used to calculate the acoustic radiation force F_{ac} , applicable to any sound field. The primary acoustic radiation force F_{ac} is defined as a function of a field potential U ,

$$F_{ac} = -\nabla(U),$$

where the field potential U is defined as

$$U = V_0 \left[\frac{\langle p^2 \rangle}{2\rho_f c_f^2} f_1 - \frac{3\rho_f \langle u^2 \rangle}{4} f_2 \right],$$

and f_1 and f_2 are the monopole and dipole contributions defined by

$$f_1 = 1 - \frac{1}{\Lambda \sigma^2}, f_2 = \frac{2(\Lambda - 1)}{2\Lambda + 1},$$

where p is the acoustic pressure, u is the fluid particle velocity, Λ is the ratio of cell density ρ_p to fluid density ρ_f , σ is the ratio of cell sound speed c_p to fluid sound speed c_f .

V_o is the volume of the cell, and $\langle \rangle$ indicates time averaging over the period of the wave. Gor'kov's formulation applies to particles smaller than the wavelength. For larger particle sizes, Ilinskii provides equations for calculating the 3D acoustic radiation forces for any particle size. See Ilinskii, *Acoustic Radiation Force on a Sphere in Tissue*, The Journal of the Acoustical Society of America, 132, 3, 1954 (2012), which is incorporated herein by reference.

Perturbation of the piezoelectric crystal in an ultrasonic transducer in a multimode fashion allows for generation of a multidimensional acoustic standing wave. A piezoelectric crystal can be specifically designed to deform in a multimode fashion at designed frequencies, allowing for generation of a multi-dimensional acoustic standing wave. The multi-dimensional acoustic standing wave may be generated by distinct modes of the piezoelectric crystal such as the 3x3 mode that would generate multidimensional acoustic standing waves. A multitude of multidimensional acoustic standing waves may also be generated by allowing the piezoelectric crystal to vibrate through many different mode shapes. Thus, the crystal would excite multiple modes such as a 0x0 mode (i.e. a piston mode) to a 1x1, 2x2, 1x3, 3x1, 3x3, and other higher order modes and then cycle back through the lower modes of the crystal (not necessarily in straight order). This switching or dithering of the crystal between modes allows for various multidimensional wave shapes, along with a single piston mode shape to be generated over a designated time.

In the present disclosure, a single ultrasonic transducer contains a rectangular array of piezoelectric elements, which can be operated such that some components of the array will be out of phase with other components of the array. This can also separate materials in a fluid stream.

One specific application for the acoustophoresis device is in the processing of bioreactor materials. In a fed batch bioreactor, it is important at the end of the production cycle to filter all of the cells and cell debris from the expressed materials that are in the fluid stream. The expressed materials are composed of biomolecules such as recombinant proteins or monoclonal antibodies, and are the desired product to be recovered. Through the use of acoustophoresis, the separation of the cells and cell debris is very efficient and leads to very little loss of the expressed materials. This is an improvement over the current filtration processes (depth filtration, tangential flow filtration, centrifugation), which show limited efficiencies at high cell densities, so that the loss of the expressed materials in the filter beds themselves can be up to 5% of the materials produced by the bioreactor. The use of mammalian cell culture include Chinese hamster ovary (CHO), NS0 hybridoma cells, baby hamster kidney (BHK) cells, and human cells has proven to be a very efficacious way of producing/expressing the recombinant proteins and monoclonal antibodies required of today's pharmaceuticals. The filtration of the mammalian cells and the mammalian cell debris through acoustophoresis aids in greatly increasing the yield of the fed batch bioreactor. The acoustophoresis process, through the use of multidimensional acoustic waves, may also be coupled with a standard filtration process upstream or downstream, such as depth filtration using diatomaceous earth, tangential flow filtration (TFF), or other physical filtration processes.

Another type of bioreactor, a perfusion reactor, uses continuous expression of the target protein or monoclonal antibodies from the CHO cells. This enables a much smaller footprint in faster production cycle. The use of acoustophoresis to hold the CHO cells in a fluid stream as they are producing/expressing the proteins is a very efficient and

closed loop way of production. It also allows for a maximum production efficiency of the proteins and monoclonal antibodies in that none of the materials are lost in a filter bed.

In the fed batch bioreactor process, the acoustophoresis device uses singular or multiple standing waves to trap the cells and cell debris. The cells and cell debris, having a positive contrast factor, move to the nodes (as opposed to the anti-nodes) of the standing wave. As the cells and cell debris agglomerate at the nodes of the standing wave, there is also a physical scrubbing of the fluid stream that occurs whereby more cells are trapped as they come in contact with the cells that are already held within the standing wave. When the cells in the multi-dimensional acoustic standing wave agglomerate to the extent where the mass is no longer able to be held by the acoustic wave, the aggregated cells and cell debris that have been trapped fall out of the fluid stream through gravity, and can be collected separately. This is a continuous process of gravitational separation.

Advanced multi-physics and multiple length scale computer models and high frequency (MHz), high-power, and high-efficiency ultrasonic drivers with embedded controls have been combined to arrive at new designs of acoustic resonators driven by arrays of piezoelectric transducers, resulting in acoustophoretic separation devices that far surpass current capabilities.

Desirably, such transducers generate a multi-dimensional acoustic standing wave in the fluid that exerts a lateral force on the suspended particles/secondary fluid to accompany the axial force so as to increase the particle trapping capabilities of an acoustophoretic system. Typical results published in literature state that the lateral force is two orders of magnitude smaller than the axial force. In contrast, the technology disclosed in this application provides for a lateral force to be of the same order of magnitude as the axial force.

The system is driven by a control signal and amplifier (not shown). The system performance is monitored and controlled by a computer. It may be necessary, at times, due to acoustic streaming, to modulate the frequency or voltage amplitude of the standing wave. This may be done by amplitude modulation and/or by frequency modulation. The duty cycle of the propagation of the standing wave may also be utilized to achieve certain results for trapping of materials. In other words, the acoustic beam may be turned on and shut off at different frequencies to achieve desired results.

The lateral force of the total acoustic radiation force (ARF) generated by the ultrasonic transducers of the present disclosure is significant and is sufficient to overcome the fluid drag force at high linear velocities up to 2 cm/s and beyond. For example, linear velocities through the devices of the present disclosure can be a minimum of 4 cm/min for separation of cells/particles, and can be as high as 2 cm/sec for separation of oil/water phases. Flow rates can be a minimum of 25 mL/min, and can range as high as 40 mL/min to 1000 mL/min, or even higher. This is true for batch reactors, fed-batch bioreactors and perfusion bioreactors.

A diagrammatic representation of an embodiment for removing oil or other lighter-than-water material is shown in FIG. 1A. Excitation frequencies typically in the range from hundreds of kHz to 10 s of MHz are applied by transducer 10. One or more standing waves are created between the transducer 10 and the reflector 11. Microdroplets 12 are trapped in standing waves at the pressure anti-nodes 14 where they agglomerate, aggregate, clump, or coalesce, and, in the case of buoyant material, float to the surface and are discharged via an effluent outlet 16 located above the flow

path. Clarified water is discharged at outlet **18**. The acoustophoretic separation technology can accomplish multi-component particle separation without any fouling at a much reduced cost.

A diagrammatic representation of an embodiment for removing contaminants or other heavier-than-water material is shown in FIG. **1B**. Excitation frequencies typically in the range from hundreds of kHz to 10 s of MHz are applied by transducer **10**. Contaminants in the incoming water **13** are trapped in standing waves at the pressure nodes **15** where they agglomerate, aggregate, clump, or coalesce, and, in the case of heavier material, sink to the bottom collector and are discharged via an effluent outlet **17** located below the flow path. Clarified water is discharged at outlet **18**.

Generally, the transducers are arranged so that they cover the entire cross-section of the flow path. The acoustophoretic separation system of FIG. **1A** or FIG. **1B** has, in certain embodiments, a square cross section of 6.375 inches×6.375 inches which operates at flow rates of up to 5 gallons per minute (GPM), or a linear velocity of 12.5 mm/sec. The transducers **10** are PZT-8 (Lead Zirconate Titanate) transducers with a 1 inch×1 inch square cross section and a nominal 2 or 3 MHz resonance frequency. Each transducer consumes about 60 W of power for droplet trapping at a flow rate of 5 GPM. This translates in an energy cost of 0.500 kW hr/m³. This is an indication of the very low cost of energy of this technology. Desirably, each transducer is powered and controlled by its own amplifier. One application for this embodiment is to shift the particle size distribution through agglomeration, aggregation, clumping or coalescing of the micron-sized oil droplets into much larger droplets.

FIG. **2** is a cross-sectional diagram of a conventional ultrasonic transducer. This transducer has a wear plate **50** at a bottom end, epoxy layer **52**, ceramic crystal **54** (made of, e.g. PZT), an epoxy layer **56**, and a backing layer **58**. On either side of the ceramic crystal, there is an electrode: a positive electrode **61** and a negative electrode **63**. The epoxy layer **56** attaches backing layer **58** to the crystal **54**. The entire assembly is contained in a housing **60** which may be made out of, for example, aluminum. An electrical adapter **62** provides connection for wires to pass through the housing and connect to leads (not shown) which attach to the crystal **54**. Typically, backing layers are designed to add damping and to create a broadband transducer with uniform displacement across a wide range of frequency and are designed to suppress excitation at particular vibrational eigenmodes. Wear plates are usually designed as impedance transformers to better match the characteristic impedance of the medium into which the transducer radiates.

FIG. **3A** is a cross-sectional view of an ultrasonic transducer **81** of the present disclosure, which can be used in acoustophoretic separator. Transducer **81** is shaped as a disc or a plate, and has an aluminum housing **82**. The piezoelectric crystal is a mass of perovskite ceramic crystals, each consisting of a small, tetravalent metal ion, usually titanium or zirconium, in a lattice of larger, divalent metal ions, usually lead or barium, and O²⁻ ions. As an example, a PZT (lead zirconate titanate) crystal **86** defines the bottom end of the transducer, and is exposed from the exterior of the housing. The crystal is supported on its perimeter by a small elastic layer **98**, e.g. silicone or similar material, located between the crystal and the housing. Put another way, no wear layer is present.

Screws **88** attach an aluminum top plate **82a** of the housing to the body **82b** of the housing via threads. The top plate includes a connector **84** for powering the transducer.

The top surface of the PZT crystal **86** is connected to a positive electrode **90** and a negative electrode **92**, which are separated by an insulating material **94**. The electrodes can be made from any conductive material, such as silver or nickel. Electrical power is provided to the PZT crystal **86** through the electrodes on the crystal. Note that the crystal **86** has no backing layer or epoxy layer as is present in FIG. **2**. Put another way, there is an air gap **87** in the transducer between aluminum top plate **82a** and the crystal **86** (i.e. the air gap is completely empty). A minimal backing **58** and/or wear plate **50** may be provided in some embodiments, as seen in FIG. **3B**.

The transducer design can affect performance of the system. A typical transducer is a layered structure with the ceramic crystal bonded to a backing layer and a wear plate. Because the transducer is loaded with the high mechanical impedance presented by the fluid, the traditional design guidelines for wear plates, e.g., half wavelength thickness for standing wave applications or quarter wavelength thickness for radiation applications, and manufacturing methods may not be appropriate. Rather, in one embodiment of the present disclosure the transducers have no wear plate or backing, allowing the crystal to vibrate in one of its eigenmodes with a high Q-factor. The vibrating ceramic crystal/disk is directly exposed to the fluid flowing through the flow chamber.

Removing the backing (e.g. making the crystal air backed) also permits the ceramic crystal to vibrate at higher order modes of vibration with little damping (e.g. higher order modal displacement). In a transducer having a crystal with a backing, the crystal vibrates with a more uniform displacement, like a piston. Removing the backing allows the crystal to vibrate in a non-uniform displacement mode. The higher order the mode shape of the crystal, the more nodal lines the crystal has. The higher order modal displacement of the crystal creates more trapping lines, although the correlation of trapping line to node is not necessarily one to one, and driving the crystal at a higher frequency will not necessarily produce more trapping lines. See the discussion below with respect to FIGS. **8-9D**.

In some embodiments, the crystal may have a backing that minimally affects the Q-factor of the crystal (e.g. less than 5%). The backing may be made of a substantially acoustically transparent material such as balsa wood, foam, or cork which allows the crystal to vibrate in a higher order mode shape and maintains a high Q-factor while still providing some mechanical support for the crystal. The backing layer may be a solid, or may be a lattice having holes through the layer, such that the lattice follows the nodes of the vibrating crystal in a particular higher order vibration mode, providing support at node locations while allowing the rest of the crystal to vibrate freely. The goal of the lattice work or acoustically transparent material is to provide support without lowering the Q-factor of the crystal or interfering with the excitation of a particular mode shape.

Placing the crystal in direct contact with the fluid also contributes to the high Q-factor by avoiding the dampening and energy absorption effects of the epoxy layer and the wear plate. Other embodiments may have wear plates or a wear surface to prevent the PZT, which contains lead, contacting the host fluid. This may be desirable in, for example, biological applications such as separating blood. Such applications might use a wear layer such as chrome, electrolytic nickel, or electroless nickel. Chemical vapor deposition could also be used to apply a layer of poly(p-xylylene) (e.g. Parylene) or other polymer. Organic and biocompatible coatings such as silicone or polyurethane are

also usable as a wear surface. A glassy carbon wear layer may also be utilized. Glassy carbon, also known as vitreous carbon, is a non-graphitizing carbon which combines both glassy and ceramic properties with those of graphite. The most important properties are high temperature resistance, hardness (7 Mohs), low density, low electrical resistance, low friction and low thermal resistance. Glassy carbon also has extreme resistance to chemical attack and impermeability to gases and liquids.

In the present disclosure, the piezoelectric crystal used in each ultrasonic transducer is modified to be in the form of a segmented array of piezoelectric elements. This array is used to form a multidimensional acoustic standing wave or waves, which can be used for acoustophoresis.

FIG. 4 shows a monolithic, one-piece, single electrode piezoelectric crystal **200** that is used in ultrasonic transducers. The piezoelectric crystal has a substantially square shape, with a length **203** and a width **205** that are substantially equal to each other (e.g. about one inch). The crystal **200** has an inner surface **202**, and the crystal also has an outer surface **204** on an opposite side of the crystal which is usually exposed to fluid flowing through the acoustophoretic device. The outer surface and the inner surface are relatively large in area, and the crystal is relatively thin (e.g. about 0.040 inches for a 2 MHz crystal).

FIG. 5 shows a piezoelectric crystal **200'** of the present disclosure. The inner surface **202** of this piezoelectric crystal **200'** is divided into a piezoelectric array **206** with a plurality of (i.e. at least two) piezoelectric elements **208**. However, the array is still a single crystal. The piezoelectric elements **208** are separated from each other by one or more channels or kerfs **210** in the inner surface **202**. The width of the channel (i.e. between piezoelectric elements) may be on the order of from about 0.001 inches to about 0.02 inches. The depth of the channel can be from about 0.001 inches to about 0.02 inches. In some instances, a potting material **212** (i.e., epoxy, Sil-Gel, and the like) can be inserted into the channels **210** between the piezoelectric elements. The potting material **212** is non-conducting, acts as an insulator between adjacent piezoelectric elements **208**, and also acts to hold the separate piezoelectric elements **208** together. Here, the array **206** contains sixteen piezoelectric elements **208** (although any number of piezoelectric elements is possible), arranged in a rectangular 4x4 configuration (square is a subset of rectangular). Each of the piezoelectric elements **208** has substantially the same dimensions as each other. The overall array **200'** has the same length **203** and width **205** as the single crystal illustrated in FIG. 4.

FIG. 6 shows another embodiment of a transducer **200''**. The transducer **200''** is substantially similar to the transducer **200'** of FIG. 5, except that the array **206** is formed from twenty-five piezoelectric elements **208** in a 5x5 configuration. Again, the overall array **200''** has the same length **203** and width **205** as the single crystal illustrated in FIG. 4.

Each piezoelectric element in the piezoelectric array of the present disclosure may have individual electrical attachments (i.e. electrodes), so that each piezoelectric element can be individually controlled for frequency and power. These elements can share a common ground electrode. This configuration allows for not only the generation of a multidimensional acoustic standing wave, but also improved control of the acoustic standing wave.

The piezoelectric array can be formed from a monolithic piezoelectric crystal by making cuts across one surface so as to divide the surface of the piezoelectric crystal into separate elements. The cutting of the surface may be performed through the use of a saw, an end mill, or other means to

remove material from the surface and leave discrete elements of the piezoelectric crystal between the channels/grooves that are thus formed.

As explained above, a potting material may be incorporated into the channels/grooves between the elements to form a composite material. For example, the potting material can be a polymer, such as epoxy. In particular embodiments, the piezoelectric elements **208** are individually physically isolated from each other. This structure can be obtained by filling the channels **210** with the potting material, then cutting, sanding or grinding the outer surface **204** down to the channels. As a result, the piezoelectric elements are joined to each other through the potting material, and each element is an individual component of the array. Put another way, each piezoelectric element is physically separated from surrounding piezoelectric elements by the potting material. FIG. 21 is a cross-sectional view comparing these two embodiments. On top, a crystal as illustrated in FIG. 5 is shown. The crystal is kerfed into four separate piezoelectric elements **208** on the inner surface **202**, but the four elements share a common outer surface **204**. On the bottom, the four piezoelectric elements **208** are physically isolated from each other by potting material **212**. No common surface is shared between the four elements.

In the present systems, the system is operated at a voltage such that the particles are trapped in the ultrasonic standing wave, i.e., remain in a stationary position. The particles are collected in along well defined trapping lines, separated by half a wavelength. Within each nodal plane, the particles are trapped in the minima of the acoustic radiation potential. The axial component of the acoustic radiation force drives the particles, with a positive contrast factor, to the pressure nodal planes, whereas particles with a negative contrast factor are driven to the pressure anti-nodal planes. The radial or lateral component of the acoustic radiation force is the force that traps the particle. In systems using typical transducers, the radial or lateral component of the acoustic radiation force is typically several orders of magnitude smaller than the axial component of the acoustic radiation force. However, the lateral force in the devices of the present disclosure can be significant, on the same order of magnitude as the axial force component, and is sufficient to overcome the fluid drag force at linear velocities of up to 1 cm/s. As discussed above, the lateral force can be increased by driving the transducer in higher order mode shapes, as opposed to a form of vibration where the crystal effectively moves as a piston having a uniform displacement. The acoustic pressure is proportional to the driving voltage of the transducer. The electrical power is proportional to the square of the voltage.

During operation, the piezoelectric arrays of the present disclosure can be driven so that the piezoelectric elements are in phase with each other. In other words, each piezoelectric element creates a multi-dimensional acoustic standing wave that has the same frequency and no time shift. In other embodiments, the piezoelectric elements can be out of phase with each other, i.e. there is a different frequency or time shift, or they have a different phase angle. As described further below, in more specific embodiments the elements in the array are arranged in groups or sets that are out of phase by multiples of 90° (i.e. 90° and/or 180°).

In embodiments, the pulsed voltage signal driving the transducer can have a sinusoidal, square, sawtooth, or triangle waveform; and have a frequency of 500 kHz to 10 MHz. The pulsed voltage signal can be driven with pulse width modulation, which produces any desired waveform.

The pulsed voltage signal can also have amplitude or frequency modulation start/stop capability to eliminate streaming.

FIG. 7 is a log-log graph (logarithmic y-axis, logarithmic x-axis) that shows the scaling of the acoustic radiation force, fluid drag force, and buoyancy force with particle radius. Calculations are done for a typical SAE-30 oil droplet used in experiments. The buoyancy force is a particle volume dependent force, and is therefore negligible for particle sizes on the order of micron, but grows, and becomes significant for particle sizes on the order of hundreds of microns. The fluid drag force scales linearly with fluid velocity, and therefore typically exceeds the buoyancy force for micron sized particles, but is negligible for larger sized particles on the order of hundreds of microns. The acoustic radiation force scaling is different. When the particle size is small, Gor'kov's equation is accurate and the acoustic trapping force scales with the volume of the particle. Eventually, when the particle size grows, the acoustic radiation force no longer increases with the cube of the particle radius, and will rapidly vanish at a certain critical particle size. For further increases of particle size, the radiation force increases again in magnitude but with opposite phase (not shown in the graph). This pattern repeats for increasing particle sizes.

Initially, when a suspension is flowing through the system with primarily small micron sized particles, it is necessary for the acoustic radiation force to balance the combined effect of fluid drag force and buoyancy force for a particle to be trapped in the standing wave. In FIG. 7 this happens for a particle size of about 3.5 micron, labeled as R_{c1} . The graph then indicates that all larger particles will be trapped as well. Therefore, when small particles are trapped in the standing wave, particles coalescence/clumping/aggregation/agglomeration takes place, resulting in continuous growth of effective particle size. As the particle size grows, the acoustic radiation force reflects off the particle, such that large particles will cause the acoustic radiation force to decrease. Particle size growth continues until the buoyancy force becomes dominant, which is indicated by a second critical particle size, R_{c2} , at which size the particles will rise or sink, depending on their relative density with respect to the host fluid. As the particles rise or sink, they no longer reflect the acoustic radiation force, so that the acoustic radiation force then increases. Not all particles will drop out, and those remaining particles will continue to grow in size as well. This phenomenon explains the quick drops and rises in the acoustic radiation force beyond size R_{c2} . Thus, FIG. 7 explains how small particles can be trapped continuously in a standing wave, aggregate into larger particles or clumps, and continuously fall out of the multi-dimensional acoustic standing wave due to gravitational separation.

The size, shape, and thickness of the transducer determine the transducer displacement at different frequencies of excitation, which in turn affects oil separation efficiency. Typically, the transducer is operated at frequencies near the thickness resonance frequency (half wavelength). Gradients in transducer displacement typically result in more places for oil to be trapped. Higher order modal displacements generate three-dimensional acoustic standing waves with strong gradients in the acoustic field in all directions, thereby creating equally strong acoustic radiation forces in all directions, leading to multiple trapping lines, where the number of trapping lines correlate with the particular mode shape of the transducer.

FIG. 8 shows the measured electrical impedance amplitude of a 1" square PZT-8 2-MHz transducer as a function of frequency in the vicinity of the 2.2 MHz transducer

resonance. The minima in the transducer electrical impedance correspond to acoustic resonances of the water column and represent potential frequencies for operation. Numerical modeling has indicated that the transducer displacement profile varies significantly at these acoustic resonance frequencies, and thereby directly affects the acoustic standing wave and resulting trapping force. Since the transducer operates near its thickness resonance, the displacements of the electrode surfaces are essentially out of phase. The typical displacement of the transducer electrodes is not uniform and varies depending on frequency of excitation. As an example, at one frequency of excitation with a single line of trapped oil droplets, the displacement has a single maximum in the middle of the electrode and minima near the transducer edges. At another excitation frequency, the transducer profile has multiple maxima leading to multiple trapped lines of oil droplets. Higher order transducer displacement patterns result in higher trapping forces and multiple stable trapping lines for the captured oil droplets.

To investigate the effect of the transducer displacement profile on acoustic trapping force and oil separation efficiencies, an experiment was repeated ten times, with all conditions identical except for the excitation frequency. Ten consecutive acoustic resonance frequencies, indicated by circled numbers 1-9 and letter A on FIG. 8, were used as excitation frequencies. These oscillations in the impedance correspond to the resonance of the acoustophoretic system. With the length of the acoustophoretic system being 2", the oscillations are spaced about 15 kHz apart. The conditions were experiment duration of 30 min, a 1000 ppm oil concentration of approximately 5-micron SAE-30 oil droplets, a flow rate of 500 ml/min, and an applied power of 20 W in a 1-inch wide x 2-inch long cross-section.

As the emulsion passed by the transducer, the trapping lines of oil droplets were observed and characterized. The characterization involved the observation and pattern of the number of trapping lines across the fluid channel, as shown in FIG. 9A, for seven of the ten resonance frequencies identified in FIG. 8.

FIG. 9B shows an isometric view of the system in which the trapping line locations are being determined. FIG. 9C is a view of the system as it appears when looking down the inlet, along arrow 114. FIG. 9D is a view of the system as it appears when looking directly at the transducer face, along arrow 116. The trapping lines shown in FIGS. 9B-9D are those produced at frequency 4 in FIG. 8 and FIG. 9A.

The effect of excitation frequency clearly determines the number of trapping lines, which vary from a single trapping line at the excitation frequency of acoustic resonance 5 and 9, to nine trapping lines for acoustic resonance frequency 4. At other excitation frequencies four or five trapping lines are observed. Different displacement profiles of the transducer can produce different (more) trapping lines in the standing waves, with more gradients in displacement profile generally creating higher trapping forces and more trapping lines.

Table 1 summarizes the findings from an oil trapping experiment using a system similar to FIG. 10A. An important conclusion is that the oil separation efficiency of the acoustic separator is directly related to the mode shape of the transducer. Higher order displacement profiles generate larger acoustic trapping forces and more trapping lines resulting in better efficiencies. A second conclusion, useful for scaling studies, is that the tests indicate that capturing 5 micron oil droplets at 500 ml/min requires 10 Watts of power per square-inch of transducer area per 1" of acoustic beam span. The main dissipation is that of thermo-viscous absorp-

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tion in the bulk volume of the acoustic standing wave. The cost of energy associated with this flow rate is 0.500 kWh per cubic meter.

TABLE 1

Trapping Pattern Capture Efficiency Study					
Resonance Peak Location	Total Power Input (Watts)	# of Trapping Lines	Flow rate (ml/min)	Duration (min)	Capture Efficiency (%)
4	20	9	500	30	91%
8	20	5	500	30	58%
A	20	4	500	30	58%
9	20	2	500	30	37%

A 4" by 2.5" flow cross sectional area intermediate scale apparatus **124** for separating a host fluid from a buoyant fluid or particulate is shown in FIG. **10A**. The acoustic path length is 4". The apparatus is shown here in an orientation where the flow direction is downwards, which is used for separating less-dense particles from the host fluid. However, the apparatus may be essentially turned upside down to allow separation of particles which are heavier than the host fluid. Instead of a buoyant force in an upward direction, the weight of the agglomerated particles due to gravity pulls them downward. It should be noted that this embodiment is depicted as having an orientation in which fluid flows vertically. However, it is also contemplated that fluid flow may be in a horizontal direction, or at an angle.

A particle-containing fluid enters the apparatus through inlets **126** into an annular plenum **131**. The annular plenum has an annular inner diameter and an annular outer diameter. It is noted that the term "annular" is used here to refer to the area between two shapes, and the plenum does not need to be circular. Two inlets are visible in this illustration, though it is contemplated that any number of inlets may be provided as desired. In particular embodiments, four inlets are used. The inlets are radially opposed and oriented.

A contoured nozzle wall **129** reduces the outer diameter of the flow path in a manner that generates higher velocities near the wall region and reduces turbulence, producing near plug flow as the fluid velocity profile develops, i.e. the fluid is accelerated downward in the direction of the centerline with little to no circumferential motion component and low flow turbulence. This generates a chamber flow profile that is optimum for acoustic separation and particle collection. The fluid passes through connecting duct **127** and into a flow/separation chamber **128**. As seen in the zoomed-in contoured nozzle **129** in FIG. **10B**, the nozzle wall also adds a radial motion component to the suspended particles, moving the particles closer to the centerline of the apparatus and generating more collisions with rising, buoyant agglomerated particles. This radial motion will allow for optimum scrubbing of the particles from the fluid in the connecting duct **127** prior to reaching the separation chamber. The contoured nozzle wall **129** directs the fluid in a manner that generates large scale vortices at the entrance of the collection duct **133** to also enhance particle collection. Generally, the flow area of the device **124** is designed to be continually decreasing from the annular plenum **131** to the separation chamber **128** to assure low turbulence and eddy formation for better particle separation, agglomeration, and collection. The nozzle wall has a wide end and a narrow end. The term scrubbing is used to describe the process of particle/droplet agglomeration, aggregation, clumping or coalescing, that occurs when a larger particle/droplet travels in a direction

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opposite to the fluid flow and collides with smaller particles, in effect scrubbing the smaller particles out of the suspension.

Returning to FIG. **10A**, the flow/separation chamber **128** includes a transducer array **130** and reflector **132** on opposite sides of the chamber. In use, multi-dimensional standing waves **134** are created between the transducer array **130** and reflector **132**. These standing waves can be used to agglomerate particles, and this orientation is used to agglomerate particles that are buoyant (e.g. oil). Fluid, containing residual particles, then exits through flow outlet **135**.

As the buoyant particles agglomerate, they eventually overcome the combined effect of the fluid flow drag forces and acoustic radiation force, and their buoyant force **136** is sufficient to cause the buoyant particles to rise upwards. In this regard, a collection duct **133** is surrounded by the annular plenum **131**. The larger particles will pass through this duct and into a collection chamber **140**. This collection chamber can also be part of an outlet duct. The collection duct and the flow outlet are on opposite ends of the apparatus.

It should be noted that the buoyant particles formed in the separation chamber **128** subsequently pass through the connecting duct **127** and the nozzle wall **129**. This causes the incoming flow from the annular plenum to flow over the rising agglomerated particles due to the inward radial motion imparted by the nozzle wall.

The transducer setup of the present disclosure creates a three dimensional pressure field which includes standing waves perpendicular to the fluid flow. The pressure gradients are large enough to generate acoustophoretic forces orthogonal to the standing wave direction (i.e., the acoustophoretic forces are parallel to the fluid flow direction) which are of the same order of magnitude as the acoustophoretic forces in the wave direction. This permits enhanced particle trapping, clumping and collection in the flow chamber and along well-defined trapping lines, as opposed to merely trapping particles in collection planes as in conventional devices. The particles have significant time to move to nodes or anti-nodes of the standing waves, generating regions where the particles can concentrate, agglomerate, and/or coalesce, and then buoyancy/gravity separate.

In some embodiments, the fluid flow has a Reynolds number of up to 1500, i.e. laminar flow is occurring. For practical application in industry, the Reynolds number is usually from 10 to 1500 for the flow through the system. The particle movement relative to the fluid motion generates a Reynolds number much less than 1.0. The Reynolds number represents the ratio of inertial flow effects to viscous effects in a given flow field. For Reynolds numbers below 1.0, viscous forces are dominant in the flow field. This results in significant damping where shear forces are predominant throughout the flow. This flow where viscous forces are dominant is called Stokes flow. The flow of molasses is an example. Wall contouring and streamlining have very little importance under such conditions. This is associated with the flow of very viscous fluids or the flow in very tiny passages, like MEMS devices. Inlet contouring has little importance. The flow of the particles relative to the fluid in an acoustophoretic particle separator will be Stokes flow because both the particle diameters and the relative velocities between the particles and fluid are very small. On the other hand, the Reynolds number for the flow through the system will be much greater than 1.0 because the fluid velocity and inlet diameter are much larger.

For Reynolds numbers much greater than 1.0, viscous forces are dominant only where the flow is in contact with

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the surface. This viscous region near the surface is called a boundary layer and was first recognized by Ludwig Prandtl. In duct flow, the flow will be laminar if the Reynolds number is significantly above 1.0 and below 2300 for fully developed flow in the duct. The wall shear stress at the wall will diffuse into the stream with distance. At the inlet of the duct, flow velocity starts off uniform. As the flow moves down the duct, the effect of wall viscous forces will diffuse inward towards the centerline to generate a parabolic velocity profile. This parabolic profile will have a peak value that is twice the average velocity. The length required for the parabolic profile to develop is a function of the Reynolds number. For a Reynolds number of 20, which is typical for CHO operation, the development length will be 1.2 duct diameters. Thus, fully developed flow happens very quickly. This peak velocity in the center can be detrimental to acoustic particle separation. Also, at laminar flow Reynolds numbers turbulence, can occur and flow surface contouring is very important in controlling the flow. For these reasons, the separator was designed with an annular inlet plenum and collector tube.

The large annular plenum is followed by an inlet wall nozzle that accelerates and directs the fluid inward toward the centerline as shown in FIG. 10B. The wall contour will have a large effect on the profile. The area convergence increases the flow average velocity, but it is the wall contour that determines the velocity profile. The nozzle wall contour will be a flow streamline, and is designed with a small radius of curvature in the separator.

The transducer(s) is/are used to create a pressure field that generates forces of the same order of magnitude both orthogonal to the standing wave direction and in the standing wave direction. When the forces are roughly the same order of magnitude, particles of size 0.1 microns to 300 microns will be moved more effectively towards regions of agglomeration ("trapping lines"). Because of the equally large gradients in the orthogonal acoustophoretic force component, there are "hot spots" or particle collection regions that are not located in the regular locations in the standing wave direction between the transducer 130 and the reflector 132. Hot spots are located at the minima of acoustic radiation potential. Such hot spots represent particle collection locations.

One application of the acoustophoretic device is the separation of a biological therapeutic protein from the biologic cells that produce the protein. In this regard, current methods of separation require filtration or centrifugation, either of which can damage cells, releasing protein debris and enzymes into the purification process and increasing the load on downstream portions of the purification system. It is desirable to be able to process volumes having higher cell densities, because this permits collection of larger amounts of the therapeutic protein and better cost efficiencies.

FIG. 11A and FIG. 11B are exploded views showing the various parts of acoustophoretic separators. FIG. 11A has only one separation chamber, while FIG. 11B has two separation chambers.

Referring to FIG. 11A, fluid enters the separator 190 through a four-port inlet 191. An annular plenum is also visible here. A transition piece 192 is provided to create plug flow through the separation chamber 193. This transition piece includes a contoured nozzle wall, like that described above in FIG. 10A, which has a curved shape. A transducer 40 and a reflector 194 are located on opposite walls of the separation chamber. Fluid then exits the separation chamber 193 and the separator through outlet 195. The separation chamber has a rectangular-shaped flow path geometry.

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FIG. 11B has two separation chambers 193. A system coupler 196 is placed between the two chambers 193 to join them together.

Acoustophoretic separation has been tested on different lines of Chinese hamster ovary (CHO) cells. In one experiment, a solution with a starting cell density of 8.09×10^6 cells/mL, a turbidity of 1,232 NTU, and cell viability of roughly 75% was separated using a system as depicted in FIG. 11A. The transducers were 2 MHz crystals, run at approximately 2.23 MHz, drawing 24-28 Watts. A flow rate of 25 mL/min was used. The result of this experiment is shown in FIG. 12A.

In another experiment, a solution with a starting cell density of 8.09×10^6 cells/mL, a turbidity of 1,232 NTU, and cell viability of roughly 75% was separated. This CHO cell line had a bi-modal particle size distribution (at size 12 μ m and 20 μ m). The result is shown in FIG. 12B.

FIG. 12A and FIG. 12B were produced by a Beckman Coulter Cell Viability Analyzer. Other tests revealed that frequencies of 1 MHz and 3 MHz were not as efficient as 2 MHz at separating the cells from the fluid.

In other tests at a flow rate of 10 L/hr, 99% of cells were captured with a confirmed cell viability of more than 99%. Other tests at a flow rate of 50 mL/min (i.e. 3 L/hr) obtained a final cell density of 3×10^6 cells/mL with a viability of nearly 100% and little to no temperature rise. In yet other tests, a 95% reduction in turbidity was obtained at a flow rate of 6 L/hr.

Testing on the scaled unit shown in FIG. 10A-10B was performed using yeast as a simulant for CHO for the biological applications. For these tests, at a flow rate of 15 L/hr, various frequencies were tested as well as power levels. Table 2 shows the results of the testing.

TABLE 2

2.5" x 4" System results at 15 L/hr Flow rate			
Frequency (MHz)	30 Watts	37 Watts	45 Watts
2.2211	93.9	81.4	84.0
2.2283	85.5	78.7	85.4
2.2356	89.1	85.8	81.0
2.243	86.7	—	79.6

In biological applications, many parts, e.g. the tubing leading to and from the housing, inlets, exit plenum, and entrance plenum, may all be disposable, with only the transducer and reflector to be cleaned for reuse. Avoiding centrifuges and filters allows better separation of the CHO cells without lowering the viability of the cells. The form factor of the acoustophoretic separator is also smaller than a filtering system, allowing the CHO separation to be miniaturized. The transducers may also be driven to create rapid pressure changes to prevent or clear blockages due to agglomeration of CHO cells. The frequency of the transducers may also be varied to obtain optimal effectiveness for a given power.

The following examples are provided to illustrate the apparatuses, components, and methods of the present disclosure. The examples are merely illustrative and are not intended to limit the disclosure to the materials, conditions, or process parameters set forth therein.

EXAMPLES

A two-dimensional numerical model was developed for the acoustophoretic device using COMSOL simulation soft-

ware. The model is illustrated in FIG. 13. The device included an aluminum wall 222, and a stainless steel reflector 224 opposite the wall. Embedded in the wall was a piezoelectric transducer 230. As illustrated here, the transducer is in the form of a 4-element piezoelectric array. The wall 222 and the reflector 224 define a flow chamber, with arrow 225 indicating the flow direction of fluid through the chamber. The piezoelectric transducer was in direct contact with the fluid. Channels/kerfs 210 and potting material 212 are also illustrated, though potting material was not used in the simulation.

The simulation software was run, and its output was compared to published data (Barmatz, *J. Acoust. Soc. Am.* 77, 928, 1985). FIG. 14A compares the acoustic potential U. FIG. 14B compares the x-component of the acoustic radiation force (ARF). FIG. 14C compares the y-component of the ARF. FIG. 14D compares the absolute value of the ARF. In these figures, the published data is on the top, while the numerical model results are on the bottom. As can be seen here, the results of the numerical model match the published data, which validates the numerical model and subsequent calculations made therefrom.

Three different simulations were then run to model the separation of SAE 30 oil droplets from water using three different piezoelectric transducers: a 1-element transducer (i.e. single crystal), a 4-element transducer, and a 5-element transducer. The transducers were operated at the same frequency, and the following parameters were used for the oil and the water: oil particle radius (R_p)=10 μ m; oil density (ρ_p)=865 kg/m³; speed of sound in oil (c_p)=1750 m/sec; particle velocity (u_p)=0.001 kg/m-sec; water density (ρ_f)=1000 kg/m³; and speed of sound in water (c_f)=1500 m/sec. For the 4-element transducer, each channel had a width of 0.0156 inches and a depth of 0.0100 inches, and each element had a width of 0.2383 inches (total width of the transducer was one inch). For the 5-element transducer, each channel had a width of 0.0156 inches and a depth of 0.0100 inches, and each element had a width of 0.1875 inches.

FIG. 15 shows the simulation of the forces on a particle using the 1-element transducer, which is a two-dimensional representation of PZT crystal 200. FIG. 16 shows the simulation of the forces on a particle using the 4-element transducer, which is a two-dimensional representation of PZT crystal 200'. FIG. 17 shows the simulation of the forces on a particle using the 5-element transducer, which is a two-dimensional representation of PZT crystal 200". Each transducer had the same width, regardless of the number of elements. The amplitude of the multi-dimensional acoustic standing waves generated therefrom are clearly seen (lighter area is higher amplitude than darker area).

Next, simulations were run on a 4-element array to compare the effect of the phase on the waves. The flow rate was 500 mL/min, the Reynolds number of the fluid was 220, the input voltage per element was 2.5 VDC, and the DC power per element was 1 watt. In one simulation, the four elements were in a 0-180-0-180 phase (i.e. out of phase) with respect to each other. In another simulation, the four elements were all in phase with each other. The simulations were then compared to actual experiments conducted with a transducer device having a 4x4 piezoelectric array as in FIG. 18.

FIG. 19 compares the results of the out-of-phase simulation (left) with a picture (right) showing the actual results when an out-of-phase array was used in the transducer device of FIG. 18. The results are very similar. Where the amplitude is high in the simulation, trapped particles are seen in the actual picture.

FIG. 20 compares the results of the in-phase simulation (left) with a picture (right) showing the actual results when an in-phase array was used in the transducer device of FIG. 18. The results are very similar.

Additional numerical models were performed with the 4-element transducer and the 5-element transducer, either in-phase or out-of-phase in different arrangements, as described in Table 3 below, over a frequency sweep of 2.19 MHz to 2.25 MHz, for oil droplets of diameter 20 microns. Out-of-phase means that adjacent elements are excited with different phases.

FIG. 22 is a diagram illustrating the two out-of-phase modes that were simulated for the 4-element array. The left-hand side illustrates the 0-180-0-180 mode, while the right-hand side illustrated the 0-180-180-0 mode. FIG. 23 is a diagram illustrating the four out-of-phase modes that were simulated for the 5-element array. The top left picture illustrates the 0-180-0-180-0 mode. The top right picture illustrates the 0-0-180-0-0 mode. The bottom left picture illustrates the 0-180-180-180-0 mode. The bottom right picture illustrates the 0-90-180-90-0 mode.

The ratio of the lateral (x-axis) force component to the axial (y-axis) force component of the acoustic radiation force was determined over this frequency range, and the range of that ratio is listed in Table 3 below.

TABLE 3

Transducer	Phase	Ratio Min	Ratio Max
1-Element (single crystal)		~0.15	~0.75
4-Element Array	In-Phase	~0.08	~0.54
4-Element Array	(0-180-0-180)	~0.39	~0.94
4-Element Array	(0-180-180-0)	~0.39	~0.92
5-Element Array	In-Phase	~0.31	~0.85
5-Element Array	(0-180-0-180-0)	~0.41	~0.87
5-Element Array	(0-0-180-0-0)	~0.41	~0.81
5-Element Array	(0-180-180-180-0)	~0.40	~0.85
5-Element Array	(0-90-180-90-0)	~0.38	~0.81

FIG. 24 shows the normalized acoustic radiation force (ARF) from the single piezoelectric crystal simulation. The ARF value was normalized with the real power calculated with the measured voltage and current. FIG. 25 shows the ratio of the ARF components (lateral to axial) for the single piezoelectric crystal simulation over the tested frequency range. FIG. 26 shows the normalized acoustic radiation force (ARF) from the 5-element simulation. FIG. 27 shows the ratio of the ARF components (lateral to axial) for the 5-element simulation over the tested frequency range. Comparing FIG. 24 to FIG. 26, the peak ARF for the 1-element simulation is about 6e-11, while the peak ARF for the 5-element simulation is about 2e-9. Comparing FIG. 25 to FIG. 27, the ratio of the forces are also more consistent, with a variation of about 0.60 compared to about 0.40.

Generally, the 4-element and 5-element arrays produced high ratios, including some greater than 0.9. Some of the simulations also had acoustic radiation force amplitudes that were almost two orders of magnitude higher than those produced by the 1-element transducer (which served as the baseline).

Experimental 16-element arrays and 25-element arrays were then tested. The feed solution was a 3% packed cell mass yeast solution, used as a simulant for CHO cells for biological applications. For out-of-phase testing, a checkerboard pattern of 0° and 180° phases was used. For the 25-element array, 12 elements were at 180° and 13 elements were at 0°. These checkerboard patterns are illustrated in FIG. 28. The left-hand side is the 16-element array and the

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right-hand side is the 25-element array, with the different shades indicating the different phase angle.

The turbidity of the feed, concentrate, and permeate were measured after 30 minutes at various frequencies. The concentrate was the portion exiting the device that contained the concentrated yeast, along with some fluid. The permeate was the filtered portion exiting the device, which was mostly liquid with a much lower concentration of yeast. A lower turbidity indicated a lower amount of yeast. The capture efficiency was determined as (feed-permeate)/feed*100%. The feed rate was 30 mL/min, and the concentrate flow rate was 5 mL/min. The power to the transducers was set at 8 W.

Table 4 lists results for the single-element transducer, which is used as a baseline or control.

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TABLE 4

Frequency (MHz)	2.225	2.244
Concentrate (NTU)	15,400	15,400
Permeate (NTU)	262	327
Feed (NTU)	4,550	5,080
Capture Efficiency (%)	94.2	93.6

Table 5 lists results for the 16-element in-phase experiments.

TABLE 5

	Frequency (MHz)							
	2.22	2.225	2.23	2.242	2.243	2.244	2.255	2.26
Concentrate (NTU)	22,700	24,300	22,500	24,600	23,100	28,100	27,400	23,800
Permeate (NTU)	205	233	241	201	249	197	244	165
Feed (NTU)	5,080	4,850	5,100	4,830	4,810	5,080	4,940	4,830
Capture Efficiency (%)	96.0	95.2	95.3	95.8	94.8	96.1	95.1	96.6

Table 6 lists results for the 16-element out-of-phase experiments.

TABLE 6

	Frequency (MHz)							
	2.22	2.225	2.23	2.242	2.243	2.244	2.255	2.26
Concentrate (NTU)	40,900	21,400	26,000	49,300	19,100	55,800	22,100	35,000
Permeate (NTU)	351	369	382	1,690	829	761	397	581
Feed (NTU)	5,590	4,870	5,860	5,160	5,040	4,870	4,800	5,170
Capture Efficiency (%)	93.7	92.4	93.5	67.2	83.6	84.4	91.7	88.8

Comparing the 16-element array results to each other and the control, the in-phase array maintains high capture efficiency through the frequency range, while the out-of-phase array drops off quickly around 2.24 MHz. The efficiency results are very similar to the control for most in-phase tests. The in-phase efficiency was higher than the out-of-phase efficiency at every frequency.

Table 7 lists results for the 25-element in-phase experiments.

TABLE 7

	Frequency (MHz)							
	2.2190	2.2300	2.2355	2.2470	2.2475	2.2480	2.2485	2.2615
Concentrate (NTU)	13,300	19,800	20,900	21,400	13,700	17,300	19,000	19,500
Permeate (NTU)	950	669	283	1,044	1,094	1,164	688	797
Feed (NTU)	4,930	4,930	4,910	5,010	4,950	5,220	5,010	5,110
Capture Efficiency (%)	80.7	86.4	94.2	79.2	77.9	77.7	86.3	84.4

Table 8 lists results for the 25-element out-of-phase experiments.

TABLE 8

	Frequency (MHz)							
	2.2190	2.2300	2.2355	2.2470	2.2475	2.2480	2.2485	2.2615
Concentrate (NTU)	14,605	—	21,700	18,025	23,425	22,575	21,900	22,450
Permeate (NTU)	2,568	2,541	1,484	1,134	1,005	987	905	2,034
Feed (NTU)	5,610	6,020	5,200	6,010	5,880	5,840	5,860	5,880
Capture Efficiency (%)	54.2	57.8	71.5	81.1	82.9	83.1	84.6	65.4

Comparing the 25-element array results to each other and the control, both arrays are less efficient than the control. The 25-element in-phase array peaks around 95% and then drops off in both directions. The out-of-phase array peaks around 85% efficiency and drops off sharply. The efficiency results are very similar to the control. It should be noted that the high peak amplitudes found using the numerical model have not been tested experimentally.

The present disclosure has been described with reference to exemplary embodiments. Obviously, modifications and alterations will occur to others upon reading and understanding the preceding detailed description. It is intended that the present disclosure be construed as including all such modifications and alterations insofar as they come within the scope of the appended claims or the equivalents thereof.

The invention claimed is:

1. An apparatus for separating a second fluid or a particulate from a host fluid, comprising:

a flow chamber having at least one inlet and at least one outlet;

at least one ultrasonic transducer located on a wall of the flow chamber, the transducer including a piezoelectric array formed from a plurality of piezoelectric elements which can be driven by a voltage signal to create a multi-dimensional acoustic standing wave in the flow chamber; and

at least one reflector located on the wall on the opposite side of the flow chamber from the at least one ultrasonic transducer.

2. An apparatus for separating a second fluid or a particulate from a host fluid, comprising:

a flow chamber having at least one inlet and at least one outlet;

at least one ultrasonic transducer located on a wall of the flow chamber, the transducer including a piezoelectric array formed from a plurality of piezoelectric elements which can be driven by a voltage signal to create a multi-dimensional acoustic standing wave in the flow chamber; and

at least one reflector located on the wall on the opposite side of the flow chamber from the at least one ultrasonic transducer;

wherein the piezoelectric array is present on a single crystal, with one or more channels separating the piezoelectric elements from each other.

3. The apparatus of claim 2, wherein a potting material different from the piezoelectric material is present in the one or more channels.

4. The apparatus of claim 3, wherein the potting material is an epoxy.

5. The apparatus of claim 1, wherein each piezoelectric element is physically separated from surrounding piezoelectric elements by a potting material.

6. The apparatus of claim 1, wherein the piezoelectric array is a rectangular array.

7. The apparatus of claim 1, wherein each piezoelectric element has the same dimensions.

8. The apparatus of claim 1, wherein each piezoelectric element is individually connected to its own pair of electrodes.

9. The apparatus of claim 1, wherein a contoured nozzle wall is located upstream of the at least one inlet of the flow chamber.

10. A method of separating a second fluid or a particulate from a host fluid, comprising:

flowing a mixture of the host fluid and the second fluid or particulate through an apparatus, the apparatus comprising:

a flow chamber having at least one inlet and at least one outlet;

at least one ultrasonic transducer located on a wall of the flow chamber, the transducer including a piezoelectric array formed from a plurality of piezoelectric elements which can be driven by a voltage signal to create a multi-dimensional standing wave in the flow chamber; and

at least one reflector located on the wall on the opposite side of the flow chamber from the at least one ultrasonic transducer;

wherein the piezoelectric array is present on a single crystal, with one or more channels separating the piezoelectric elements from each other; and

sending voltage signals to the piezoelectric array to form a multi-dimensional acoustic standing wave that traps the second fluid or particulate against the flow of the fluid, permitting agglomeration at pressure nodes such that the second fluid or particulate increases in size and continuously falls out of the multi-dimensional acoustic standing wave through gravity separation.

11. The method of claim 10, wherein the particulate is Chinese hamster ovary (CHO) cells, NS0 hybridoma cells, baby hamster kidney (BHK) cells, or human cells.

12. The method of claim 10, wherein the piezoelectric elements are operated out of phase with each other.

13. The method of claim 10, wherein the piezoelectric elements are operated in phase with each other.

14. The method of claim 10, wherein the flow rate of the host fluid through the flow chamber is at least 25 mL/min.

15. The method of claim 10, wherein the piezoelectric elements operate at a frequency in a range of 100 kHz to 20 MHz.

16. The method of claim 10, wherein the multi-dimensional standing wave results in an acoustic radiation force having an axial force component and a lateral force component that are of the same order of magnitude.

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17. The method of claim 10, wherein the piezoelectric array is present on a single crystal, with one or more channels separating the piezoelectric elements from each other.

18. The method of claim 17, wherein a potting material different from the piezoelectric material is present in the one or more channels. 5

19. The method of claim 10, wherein each piezoelectric element is physically separated from surrounding piezoelectric elements by a potting material. 10

20. The method of claim 10, wherein each piezoelectric element is individually connected to its own pair of electrodes. 15

21. The apparatus of claim 1, wherein the piezoelectric array can directly contact fluid flowing through the flow chamber.

22. A method of separating a second fluid or a particulate from a host fluid, comprising:

flowing a mixture of the host fluid and the second fluid or particulate through an apparatus, the apparatus comprising:

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a flow chamber having at least one inlet and at least one outlet;

at least one ultrasonic transducer located on a wall of the flow chamber, the transducer including a piezoelectric array formed from a plurality of piezoelectric elements which can be driven by a voltage signal to create a multi-dimensional standing wave in the flow chamber; and

at least one reflector located on the wall on the opposite side of the flow chamber from the at least one ultrasonic transducer; and

sending voltage signals to the piezoelectric array to form a multi-dimensional acoustic standing wave that traps the second fluid or particulate against the flow of the fluid, permitting agglomeration at pressure nodes such that the second fluid or particulate increases in size and continuously falls out of the multi-dimensional acoustic standing wave through gravity separation.

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